

"Computational Fluid Dynamics Chemical Reaction Engineering IV" June 19-24, 2005 Barga, Italy

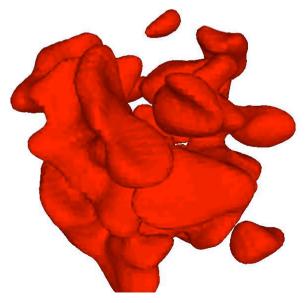
DNS and LES of Turbulent Combustion

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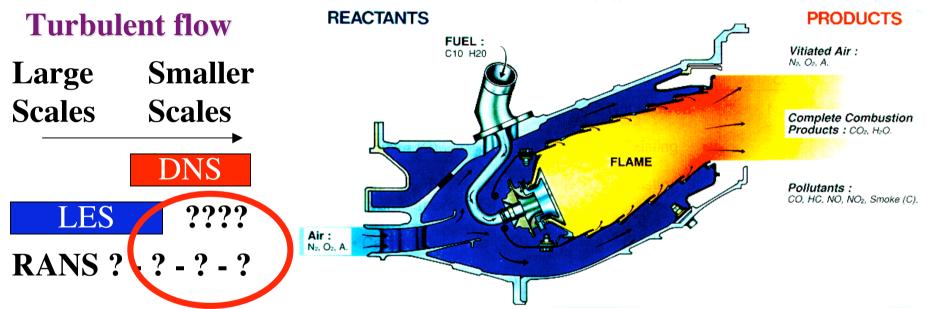






Combustion system:



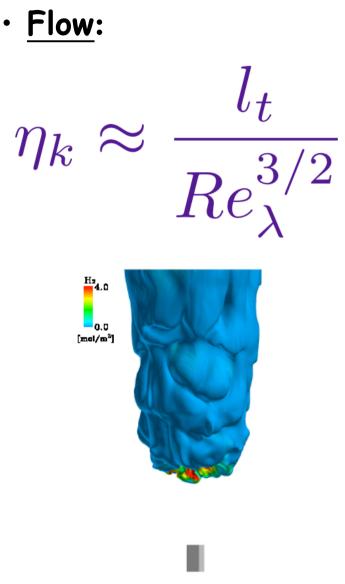


- Unsteady large scales lead to an imperfect mixing in the system. Those scales are geometry dependent and feature a long life time.
- Micro-mixing mechanisms bring reactants in ₂ contact within thin reaction zones.

OUTLINE

- \checkmark DNS of turbulent combustion.
- \checkmark Overview of turbulent combustion modeling.
- ✓ One example of SGS modeling in LES of premixed turbulent combustion.
- \checkmark SGS modeling of partially premixed combustion.

Resolution needed for full simulation:



 $10^{-6} \,\mathrm{m} < \eta_k < 10^{-4} \,\mathrm{m}$

Re_{λ}	Memory	Speed	Year
70	50 Gbytes	50 Gflops	1993
300	50 Tbytes	50 Tflops	2002
1500	50 Pbytes	50 Pflops	2015?

J. Jiménez, Eng. Turbulence Modelling and Experiments-5, 2002

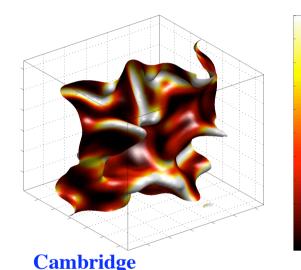
 $h \approx 5.10^{-6} \mathrm{m}$ $\Delta t \approx 1.10^{-6} \mathrm{s}$

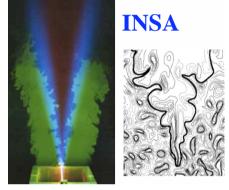
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Mizobuchi et al, Proc. Combust. Inst. 2002

So far, three types of 'full solutions' (DNS):

- DNS of synthetic model problem (freely decaying turbulence).
- DNS of laboratory flame, but at much lower Re.
- DNS of laboratory flame.







0.0 [mei/m³]

JAXA

Synthetic problem

Sandia, Livermore Laboratory flame at lower Re Real jet-flame

Chemistry:

• Single-step

15 1.4 1.3 1.2 1.1

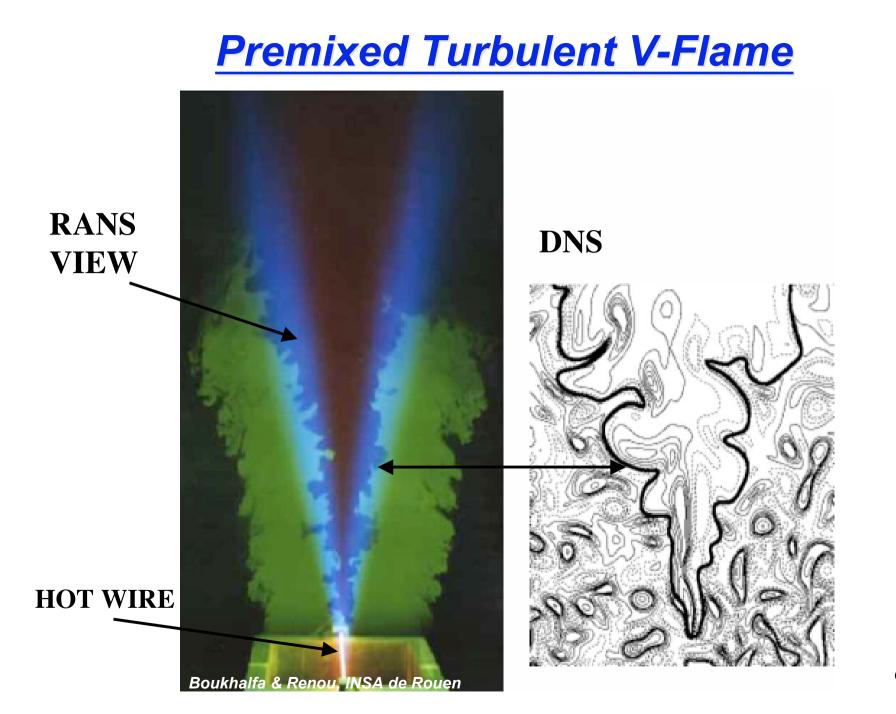
- Reduced
- Tabulated
- **Detailed**

Transport:

- Fixed Lewis and Schmidt
- Variable Lewis & Schmidt

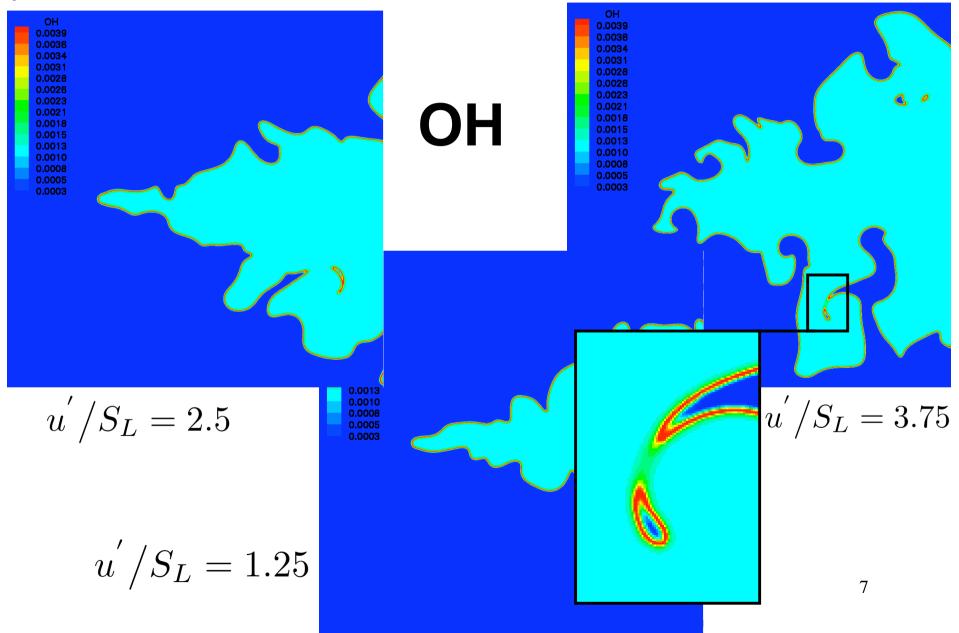
H2 4.0

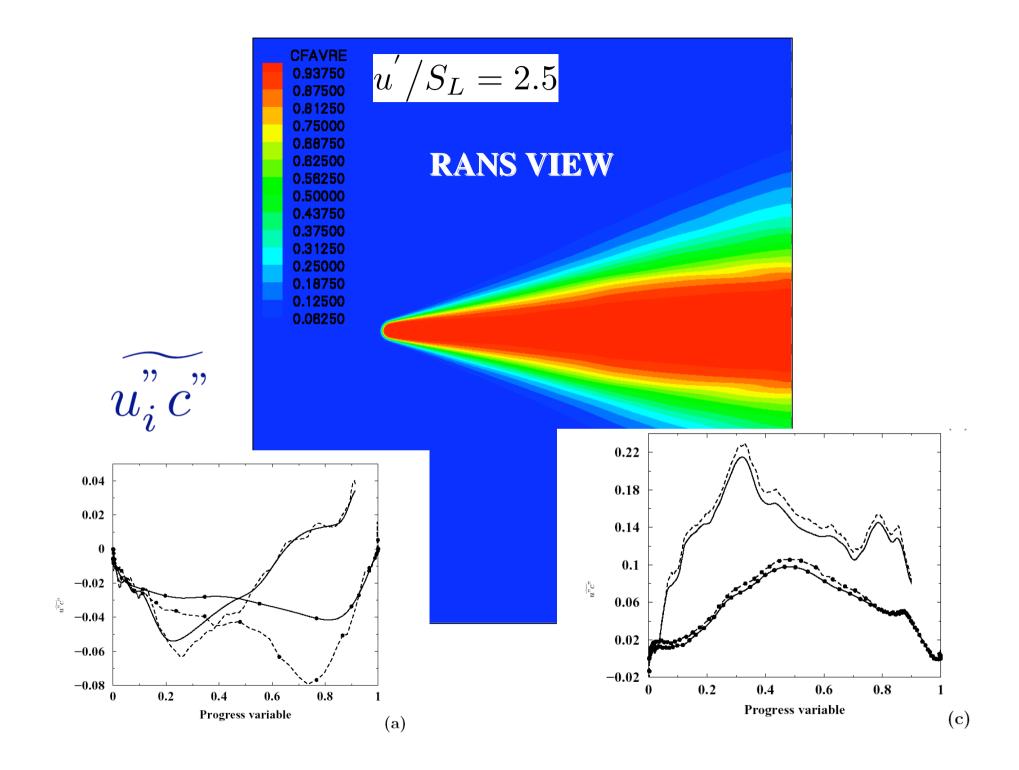
• Complex

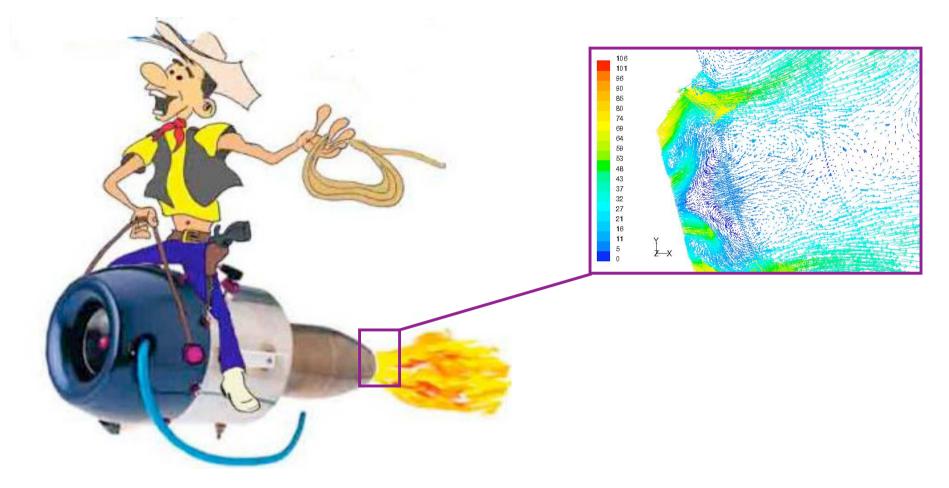


Complex chemistry FPI-FGM:

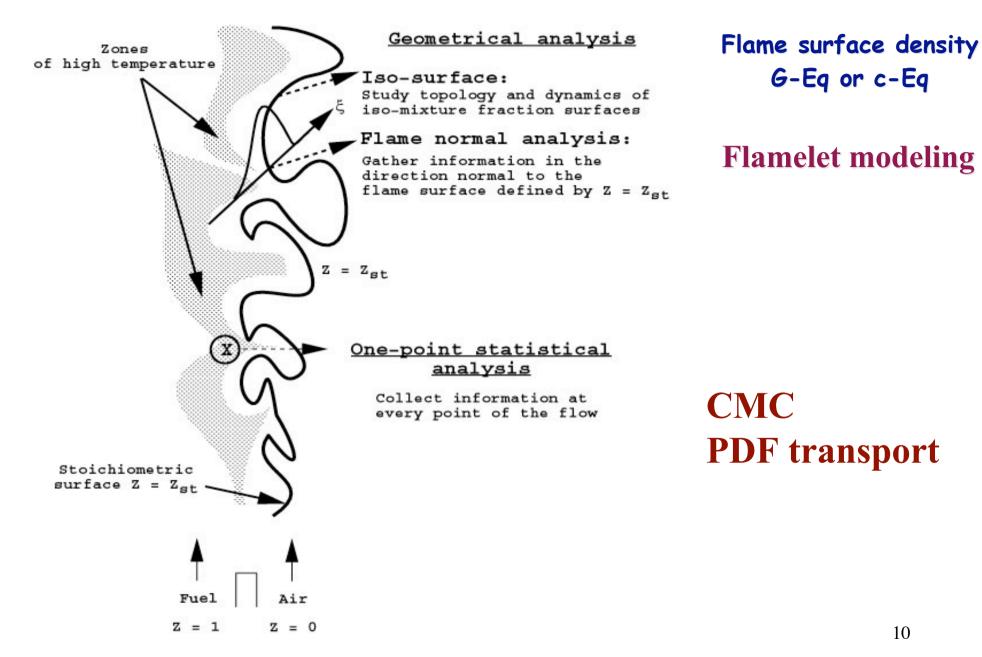
Gicquel et al Proc. Combust. Inst.Vol. 28, 1901-1908, 2000. Oijen et al Combust. Flame, 127(3):2124-2134, 2001.



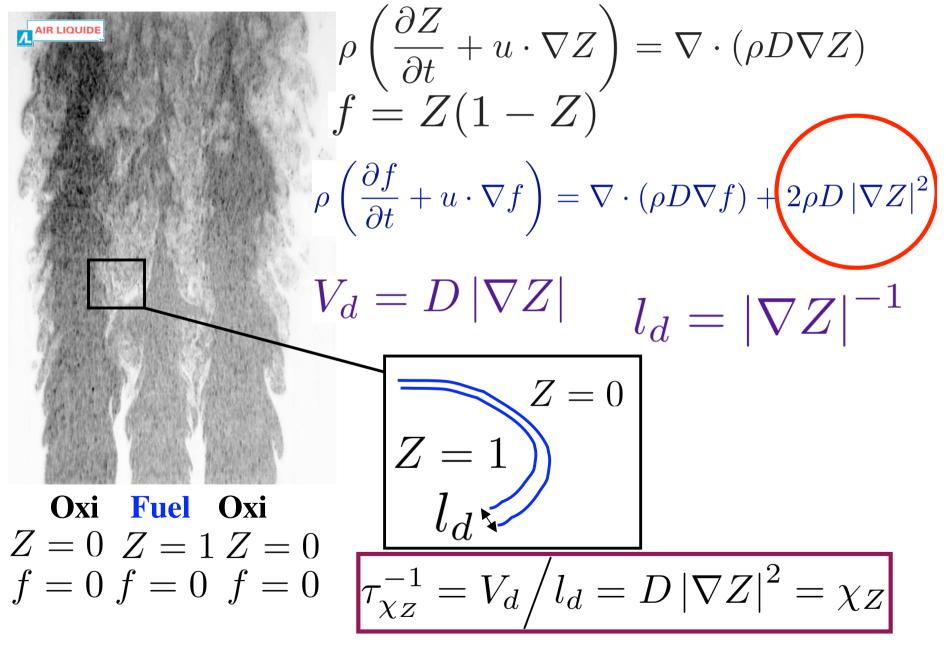


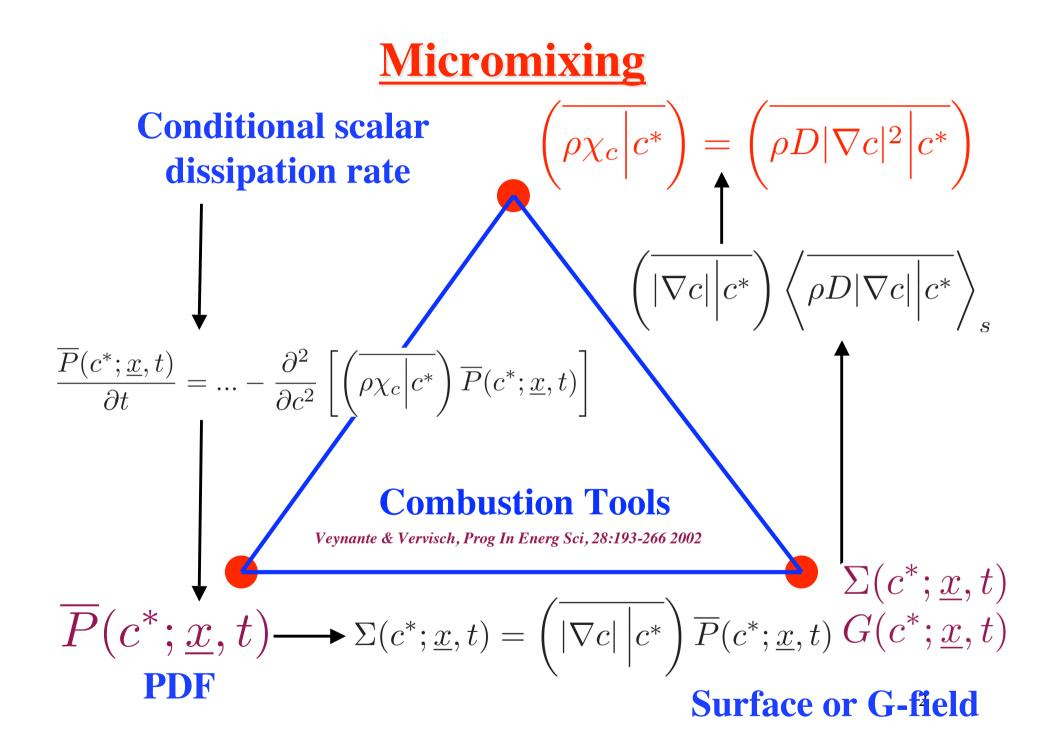


Overview of turbulent combustion modeling tools



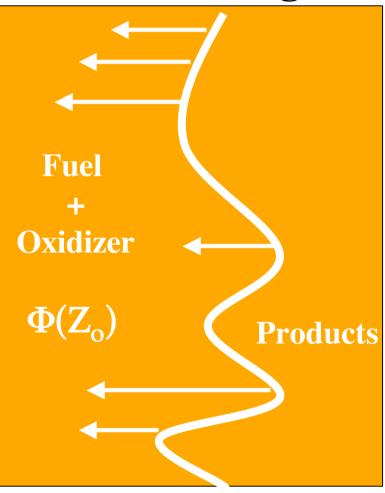
Control parameter of molecular mixing?



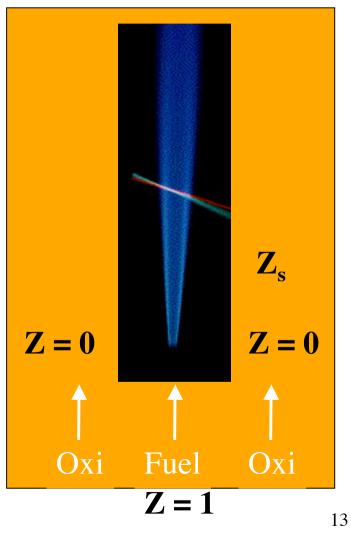


"Academic" combustion regimes

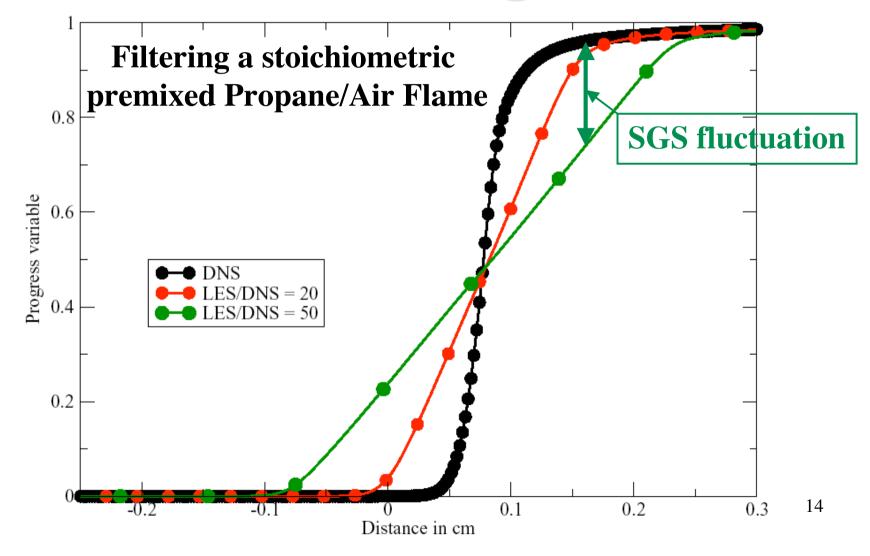
Prémélange



Diffusion



Premixed flame LES filtering



SGS Probability Density Function in premixed flames:

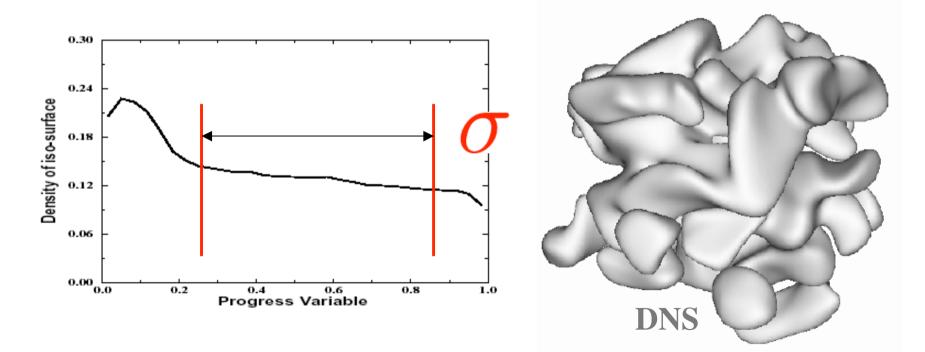
- The thin flame front has a characteristic scale within the subgrid.
- The thin flame is seen at the grid scale Δ .

EFFECTS

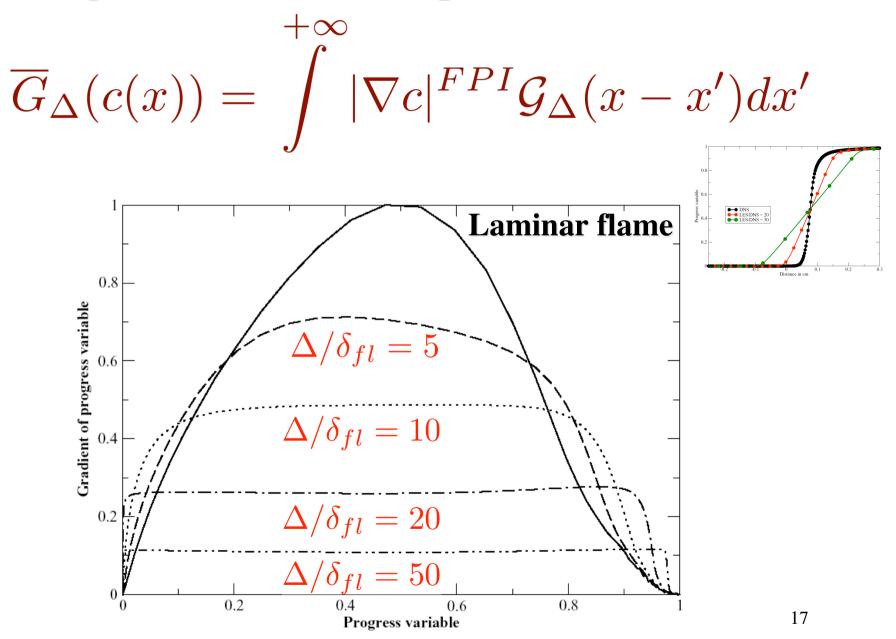
- 1. Thickening by the filter of the thin flame front over the coarse LES grid.
- 2. Wrinkling of the flame within the subgrid that results from interaction with subgrid vortices.

Flame surface density contains information on the flame characteristic length:

 $\Sigma(c^*;\underline{x},t) = \left(\overline{|\nabla c||c^*}\right)\widetilde{P}(c^*;\underline{x},t)$



Filtered gradient contains two points information



Get the PDF from the Flame Surface Density inside the flame:

$$\widetilde{P}(c^*; \underline{x}, t) = \frac{\Sigma(c^*; \underline{x}, t)}{\left(\overline{|\nabla c||c^*}\right)}$$

$$\widetilde{P}(c^*; \underline{x}, t) = \alpha(\underline{x}, t)\delta(c^*) + \beta(\underline{x}, t)\delta(1 - c^*)$$

$$+ \frac{\sigma(\underline{x}, t)}{\overline{G}_{\Delta}(c^*)}H(c^*)H(1 - c^*)$$

$$\overline{G}_{\Delta}(c(x)) = \int_{-\infty}^{+\infty} |\nabla c|^{FPI} \mathcal{G}_{\Delta}(x - x') dx'$$

Describing SGS variance of progress variable:

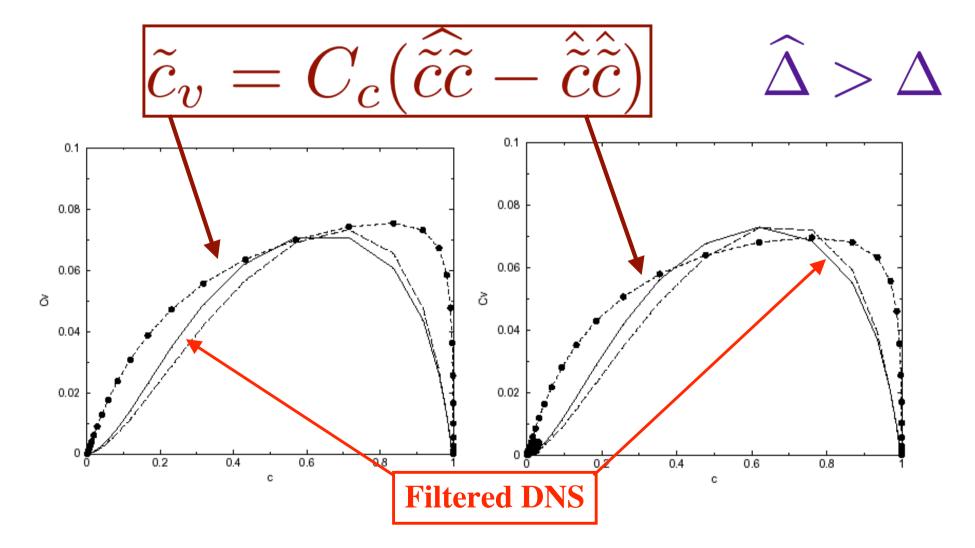
$$\widetilde{c}_v = \widetilde{c}\widetilde{c} - \widetilde{c}\widetilde{c}$$

Energy that is not resolved by the coarse LES grid.

- Try to get it from resolved scales:
 - Scale similarity hypothesis.
 - Equilibrium hypothesis.
- Solve a balance equation to get SGS variance:
 - Which balance equation is the best?
 - Close unknown terms.

$$\widetilde{c}_v = \widetilde{c}\widetilde{c} - \widetilde{c}\widetilde{c}$$

Scale similarity assumption:



 $\widetilde{c}_v = \widetilde{c}\widetilde{c} - \widetilde{c}\widetilde{c}$

Equation for SGS variance:

$$\frac{\partial \overline{\rho} \widetilde{c}_{v}}{\partial t} + \nabla \cdot (\overline{\rho} \widetilde{\mathbf{u}} \widetilde{c}_{v}) = -\nabla \cdot \overline{\tau}_{c_{v}} + \nabla \cdot (\overline{\rho} D \nabla \widetilde{c}_{v})$$

$$- 2\overline{\tau}_{c} \cdot \nabla \widetilde{c} + 2\overline{\rho} D |\nabla \widetilde{c}|^{2} - 2\overline{\rho} D |\nabla c|^{2}$$

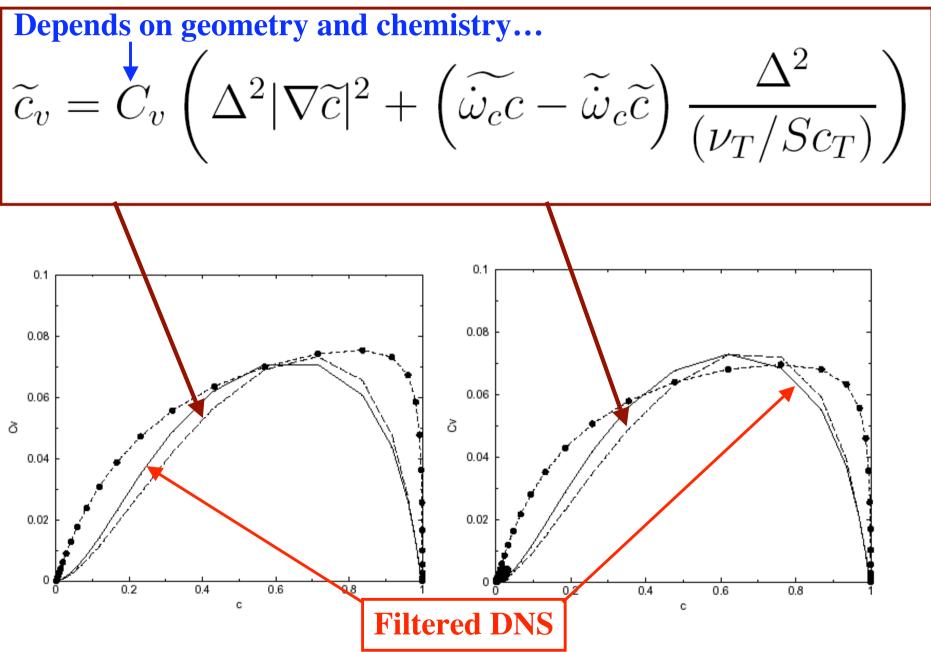
$$+ 2\overline{\rho} \left(\widetilde{\omega_{c}} c - \widetilde{\omega}_{c} \widetilde{c} \right)$$

Production - Dissipation and Source

Dissipation:
$$\overline{\rho}D|\nabla \widetilde{c}|^2 - \overline{\rho}D|\nabla c|^2 \approx -\overline{\rho}\widetilde{c}_v/\tau_t$$

 $\nu_T = (C_s \Delta)^2|\widetilde{S}| \qquad |\widetilde{S}| = (2\widetilde{S} \cdot \widetilde{S})^{1/2}$
 $\tau_t \approx \Delta^2/(\nu_T/Sc_T) \qquad \widetilde{S} = (1/2)(\nabla \widetilde{u} + \nabla^T \widetilde{u})_{21}$

Equilibrium hypothesis:



Chose the appropriate variable to be transported (the one that minimizes LES numerical problems...)

• Solve for the departure from maximum variance:

$$\widetilde{c}_{v} = \widetilde{c}\,\widetilde{c} - \widetilde{c}\,\widetilde{c} = \widetilde{c}(1 - \widetilde{c}) - \left[\widetilde{\varphi}_{c}\right]$$

$$\overline{\rho}\overline{\varphi}_{c} = \overline{\rho}c(1 - c) = \overline{\rho}\,\widetilde{c}(1 - \widetilde{c})(1 - S)$$
Unmixedness:
$$S = \frac{\widetilde{c}_{v}}{\widetilde{c}(1 - \widetilde{c})}$$

$$\widetilde{\varphi}_{c} = \frac{\widetilde{c}_{v}}{\widetilde{c}(1 - \widetilde{c})}$$

The modeled balance equations to be solved for presuming the PDF then reads:

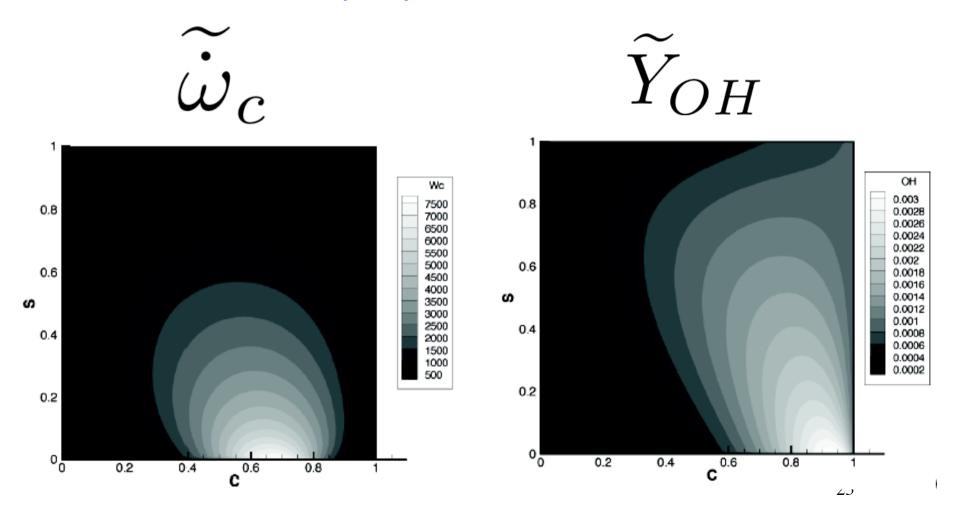
$$\frac{\partial \overline{\rho} \widetilde{c}}{\partial t} + \nabla \cdot (\overline{\rho} \widetilde{u} \widetilde{c}) = \nabla \cdot (\overline{\rho} (D + (\nu_T / S c_T)) \nabla \widetilde{c}) + \overline{\rho} \widetilde{\omega}_c$$

$$\frac{\partial \overline{\rho} \widetilde{\varphi}_c}{\partial t} + \nabla \cdot (\overline{\rho} \widetilde{u} \widetilde{\varphi}_c) = \nabla \cdot (\overline{\rho} (D + (\nu_T / S c_T)) \nabla \widetilde{\varphi}_c)$$
Scalar dissipation rate + $2\overline{\rho} \left(D |\nabla \widetilde{c}|^2 + C_D \frac{\nu_t}{S c_T} \frac{\widetilde{c}_v}{\Delta^2} \right)$
Chemical source + $\overline{\rho} \left(\widetilde{\omega}_c - 2 \widetilde{\omega}_c \widetilde{c} \right)$

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LES CHEMICAL TABLES Averaging FGM or FPI

FPI (Flame Prolongation of ILDM): Gicquel et al Proc. Combust. Inst.Vol. 28, 1901-1908, 2000. FGM (Flame Generated Manifod): Oijen et al Combust. Flame, 127(3):2124-2134, 2001.



SGE:

✓ Fully Compressible Flow.

✓ 4th ordre in space, 2nd in time.

Skew symmetric like, Ducros et al, J. Comput. Phys., 161: 114-139, 2000.

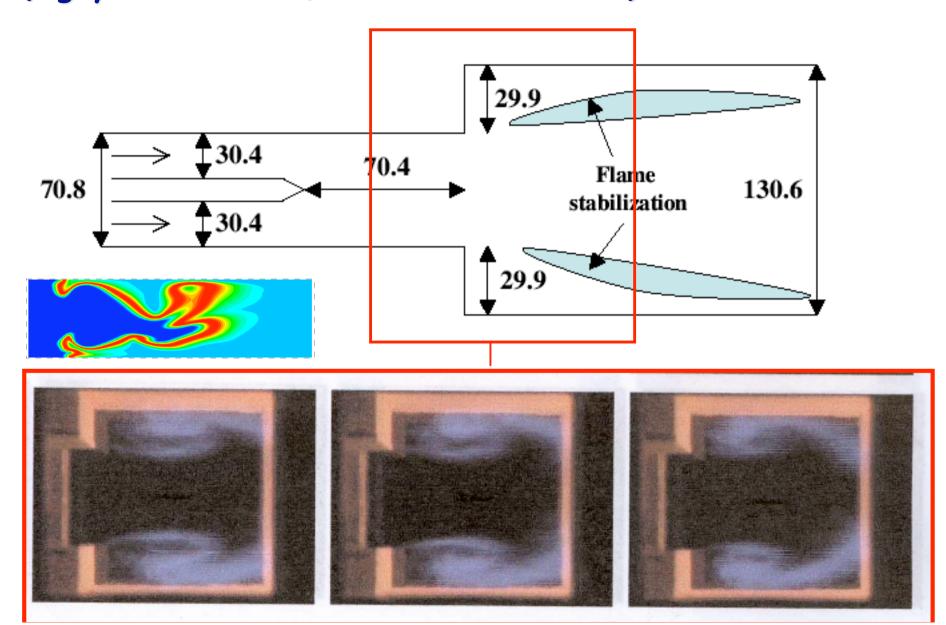
✓ Dynamic Lagrangian Modeling.

Meneveau et al, JFM, 353-386, 1996.

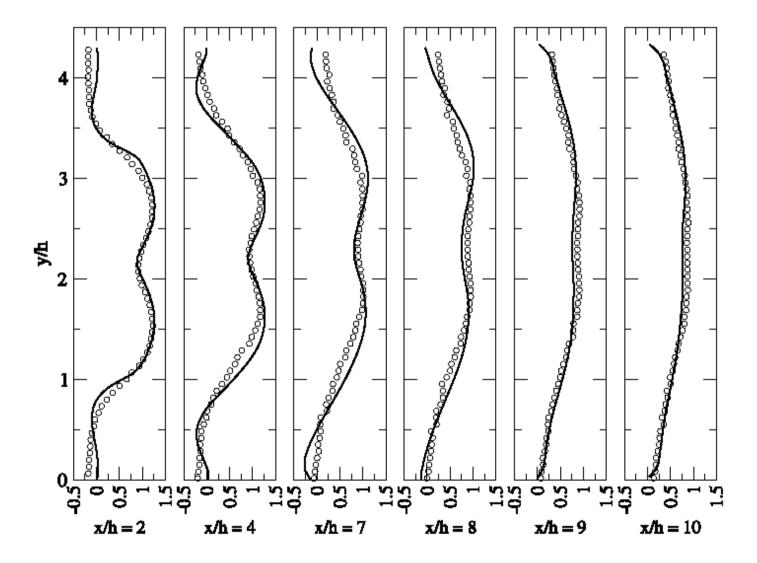


M. Lesieur Team.

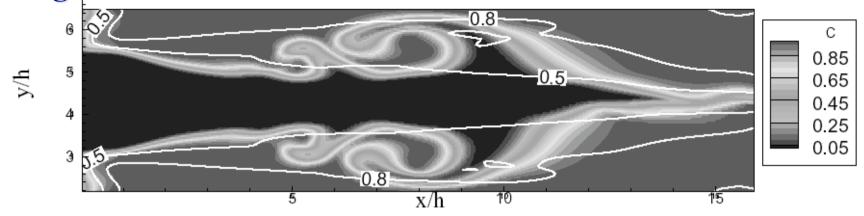
Test premixed SGS modeling on ORACLES (Nguyen and Bruel, AIAA-2003-0958.)



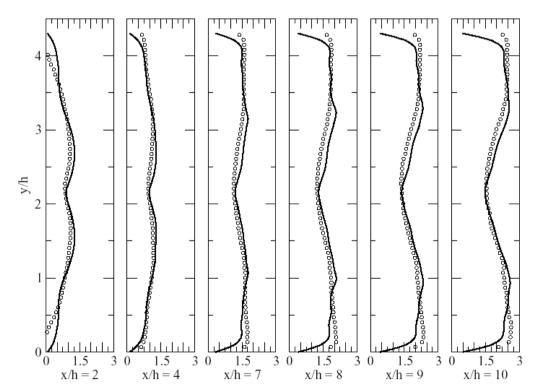
Time averaged streamwise velocity frozen flow mixing:



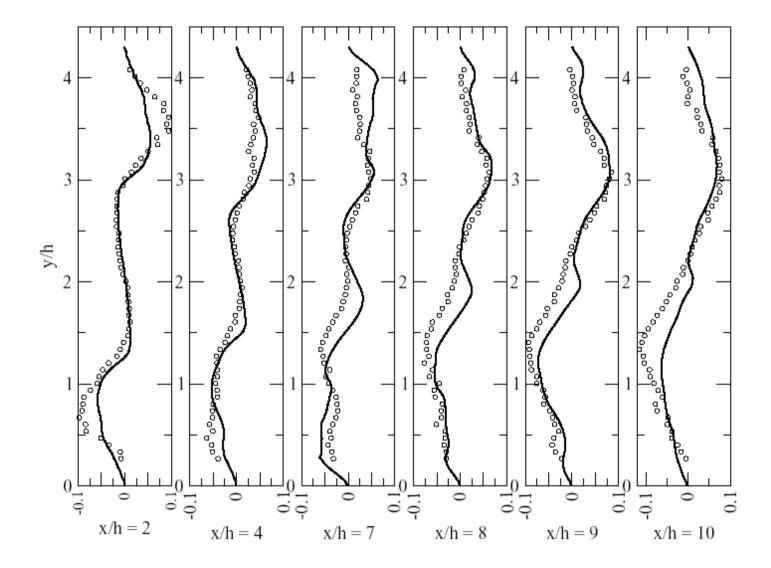
Progress variable:



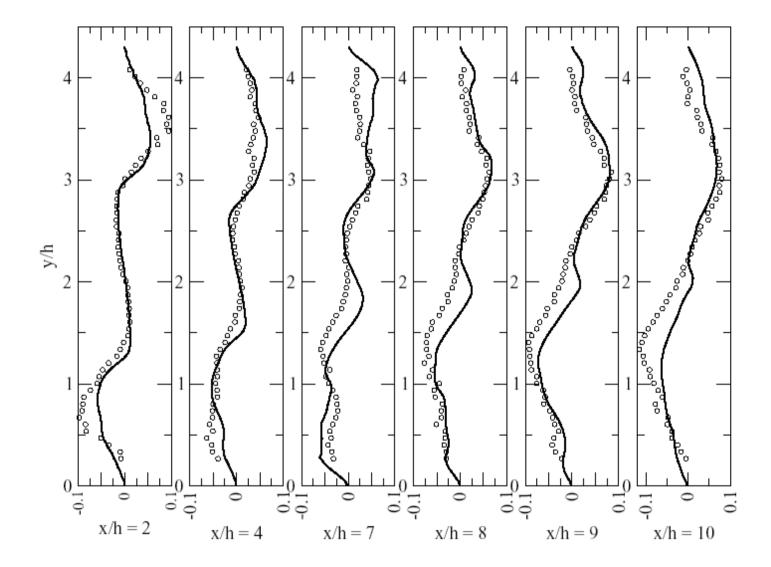
Time averaged streamwise velocity:



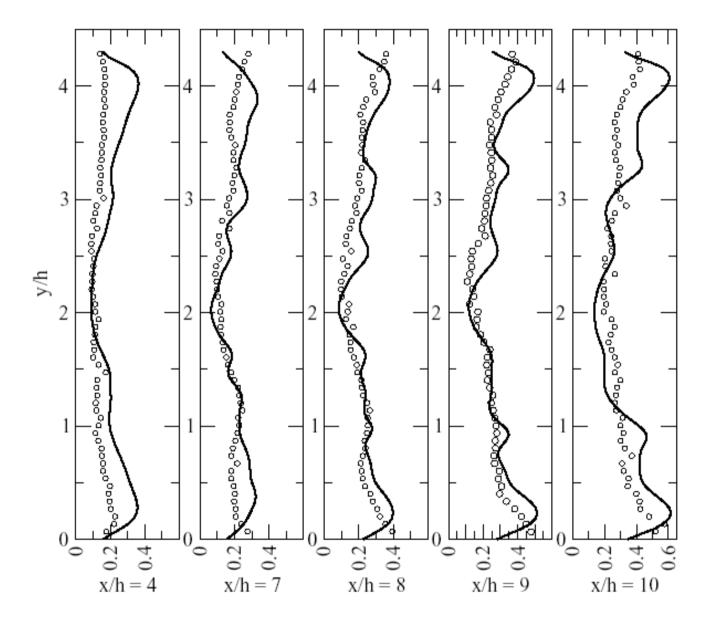
Time averaged spanwise velocity:



Time averaged spanwise velocity:



Time averaged RMS velocity:



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OUTLINE

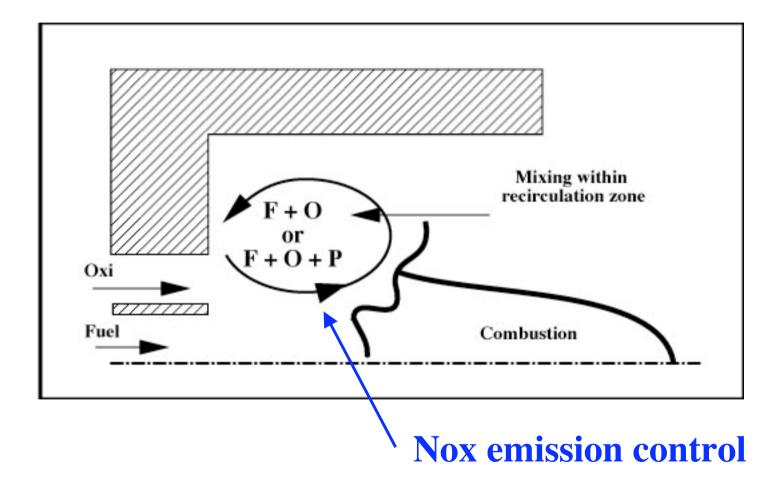
 \checkmark DNS of turbulent combustion.

✓ Overview of turbulent combustion modeling.

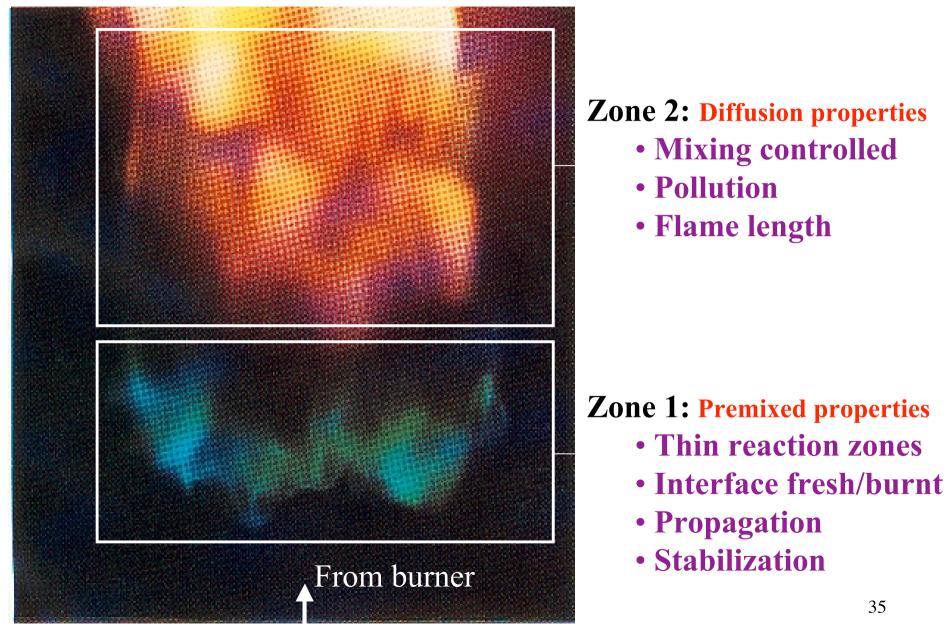
✓ One example of SGS modeling for LES of premixed turbulent combustion.

✓ SGS modeling of partially premixed combustion.

Industrial combustion

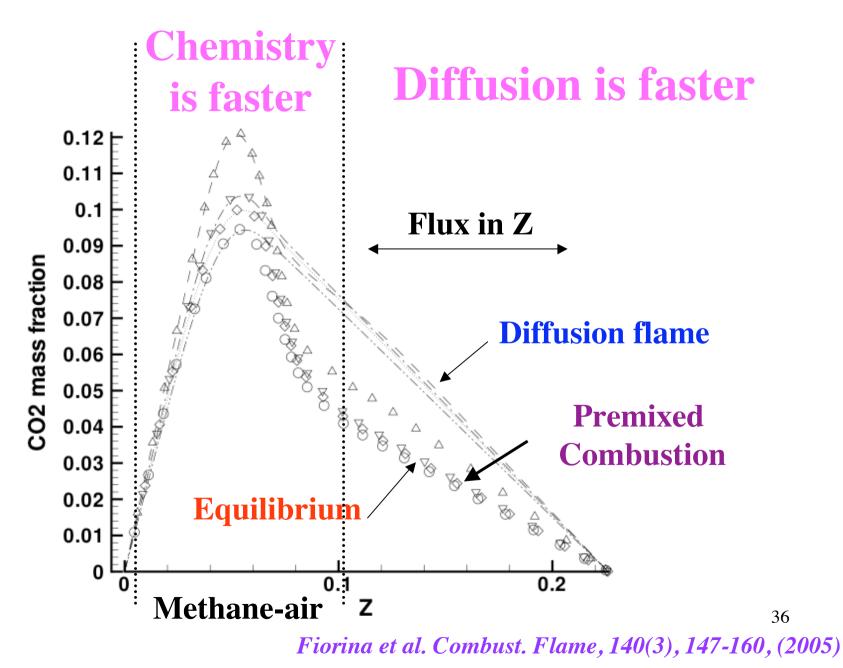


Nonpremixed turbulent flame base:



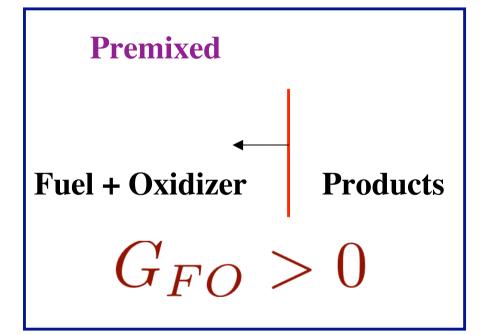
Muniz & Mungal, Combust. Flame 111(1/2), 1997

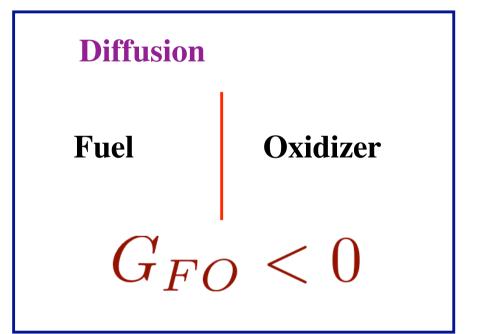
Premixed/Diffusion combustion



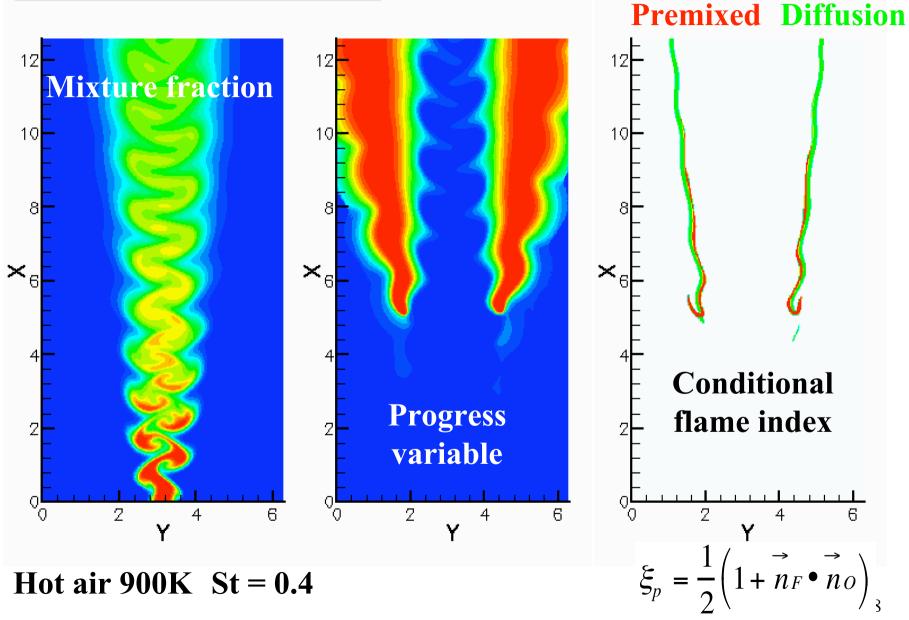
Takeno's flame index to determine combustion regime:

$$G_{FO} = \nabla Y_F \cdot \nabla Y_O$$



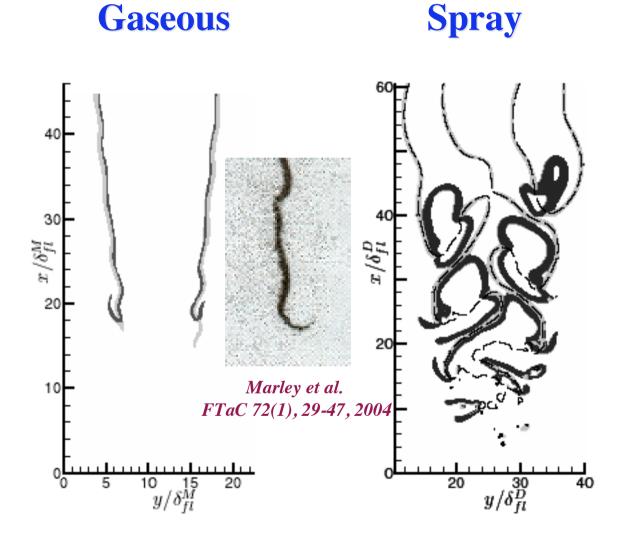


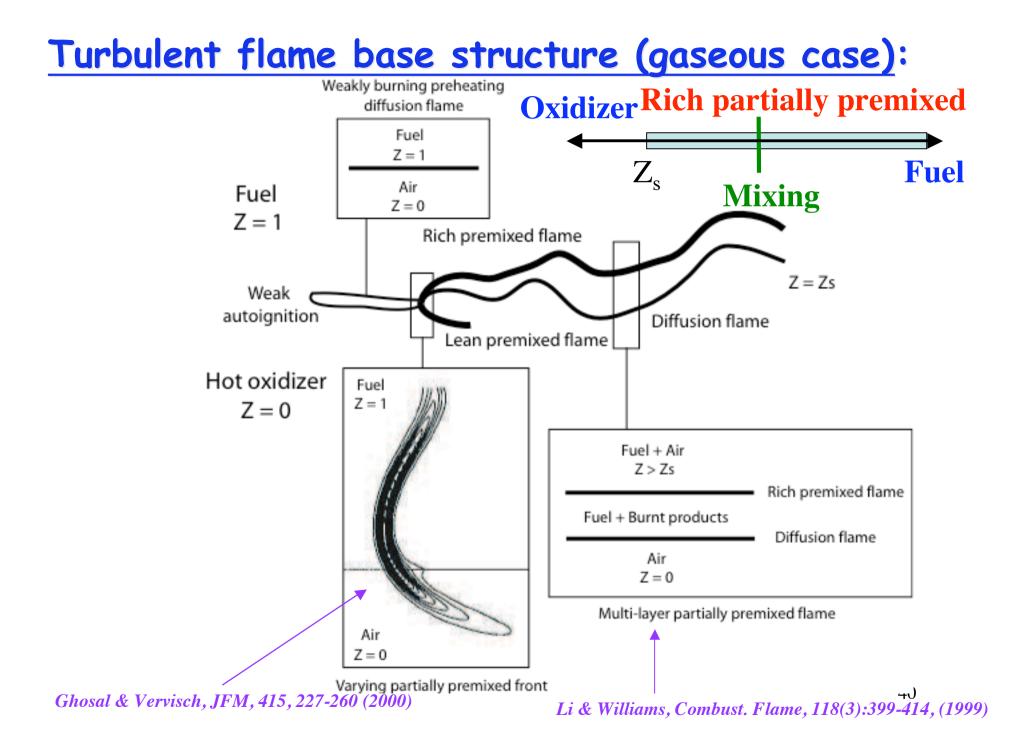
DNS of lifted flames:



Sixth order PADE, Third order time stepping, NSCBC Boundary conditions

DNS of weakly turbulent flame bases:



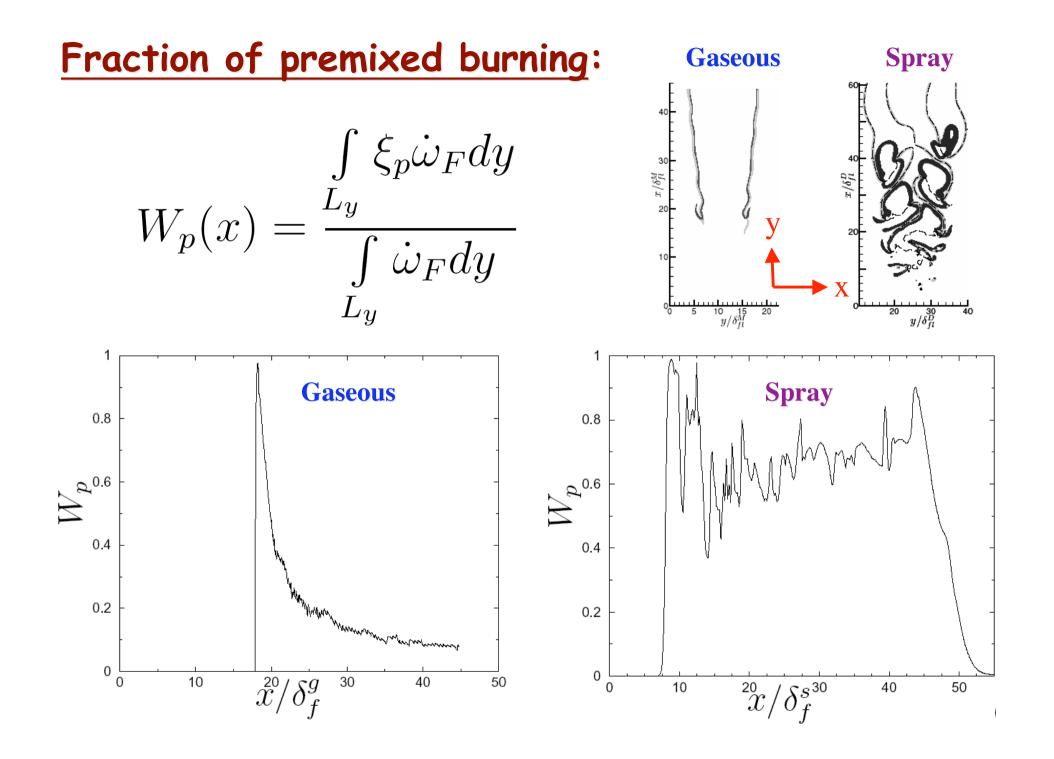


Amplitude of the burning rate in premixed mode:

$$\xi_p = \frac{1}{2} \left(1 + \frac{\nabla Y_F}{|\nabla Y_F|} \cdot \frac{\nabla Y_O}{|\nabla Y_O|} \right) = 0 \text{ Diffusion}$$

$$W_p(x) = \frac{\int_y \xi_p \dot{\omega} dy}{\int_y \dot{\omega} dy}$$

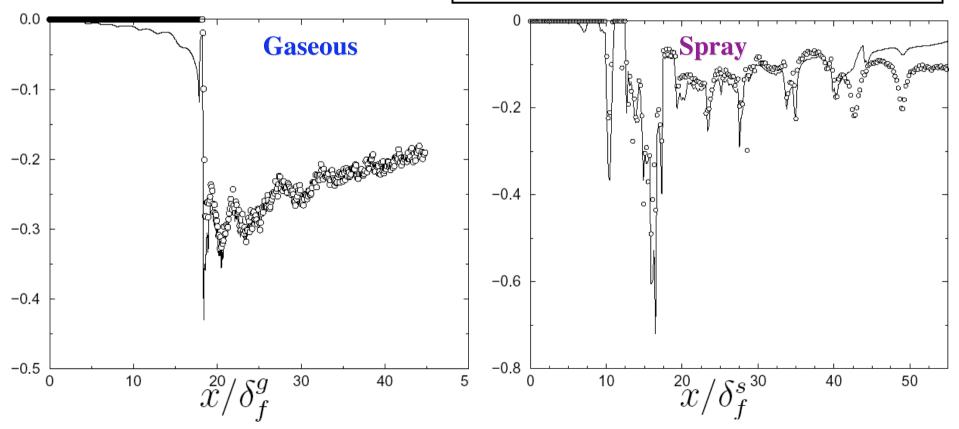
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Diffusion flamelet, but only for the "diffusion-part":

$$\chi_Z \frac{dY_F^d}{dZ^2} = -\dot{\omega}_F^d(Z,\chi_Z)$$

$$\begin{aligned} \mathcal{I}_{d}^{DNS} &= \int_{L_{y}} (1 - \xi_{p}) \dot{\omega}_{F} dy \\ \mathcal{I}_{d}^{Eq.38} &= \int_{L_{y}} (1 - \xi_{p}) \dot{\omega}_{F}^{d} (Z, \chi_{Z}) dy \end{aligned}$$



Flame decomposition:

$$\overline{\dot{\omega}}_F = \overline{\xi_p \dot{\omega}_F^p} + (1 - \xi_p) \dot{\omega}_F^d$$

Modeled decomposition:

$$\overline{\dot{\omega}}_F = \overline{\alpha}_p \overline{\dot{\omega}_F^p} + \overline{\alpha}_d \overline{\dot{\omega}_F^d}$$

Modeled coefficients:

$$\overline{\alpha}_p = \frac{\xi_p \dot{\omega}_F^p}{\overline{\dot{\omega}_F^p}} \quad \overline{\alpha}_d = \frac{(1-\xi_p) \dot{\omega}_F^d}{\overline{\dot{\omega}_F^d}}$$

Modeled decomposition:

• Domingo et al, "DNS analysis of partially premixed combustion in spray and gaseous turbulent-flame bases stabilized in hot air", Combust. Flame, 103(3): 172-195, 2005.

• Reveillon & Vervisch, "Analysis of weakly turbulent diluted-spray flames and spray combustion regimes", JFM, 537:317-347, 2005.

