



CFD Modelling of Turbulent Mass Transfer in a Mixing Channel

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Overview

Objectives

Flow Configuration

PIV/PLIF Experiment

Governing Equations

Turbulence and Micromixing Models

Numerical Results

Conclusions

Objectives

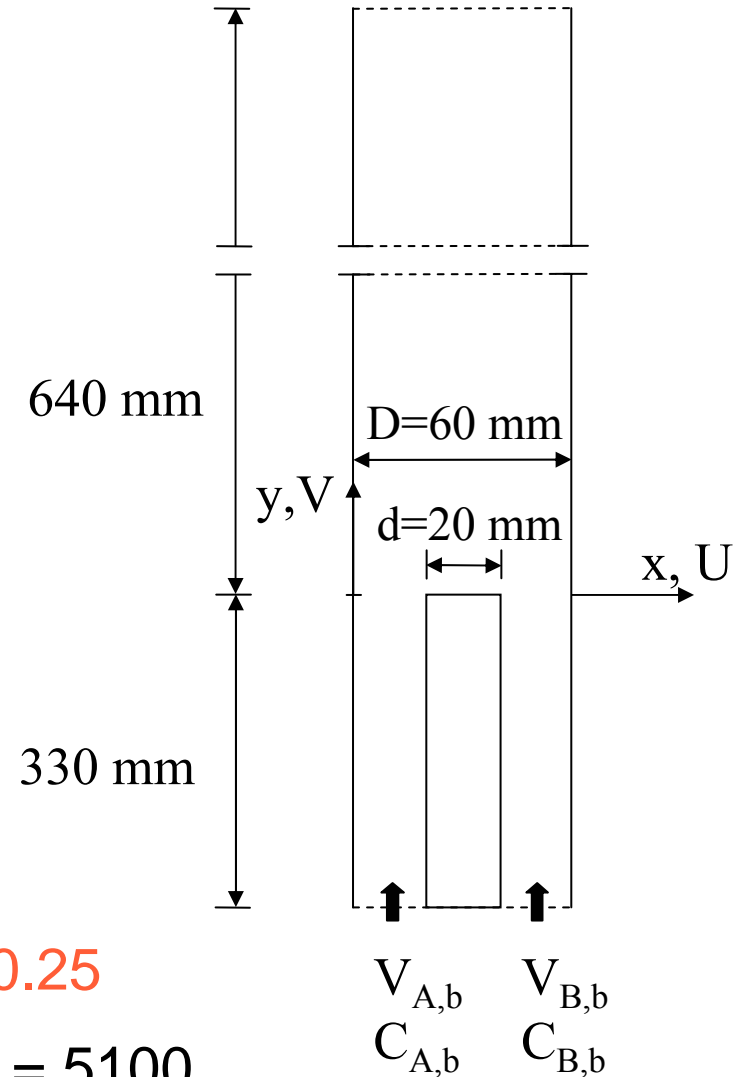
Objectives of current project

- PIV/PLIF measurements of **mass transfer** and chemical reactions in turbulent liquid flows
 - **pure mixing/mass transfer**
 - acid-base chemical reaction (Poster presentation)
- CFD modelling of **mass transfer** and chemical reactions (Poster presentation) in turbulent liquid flows

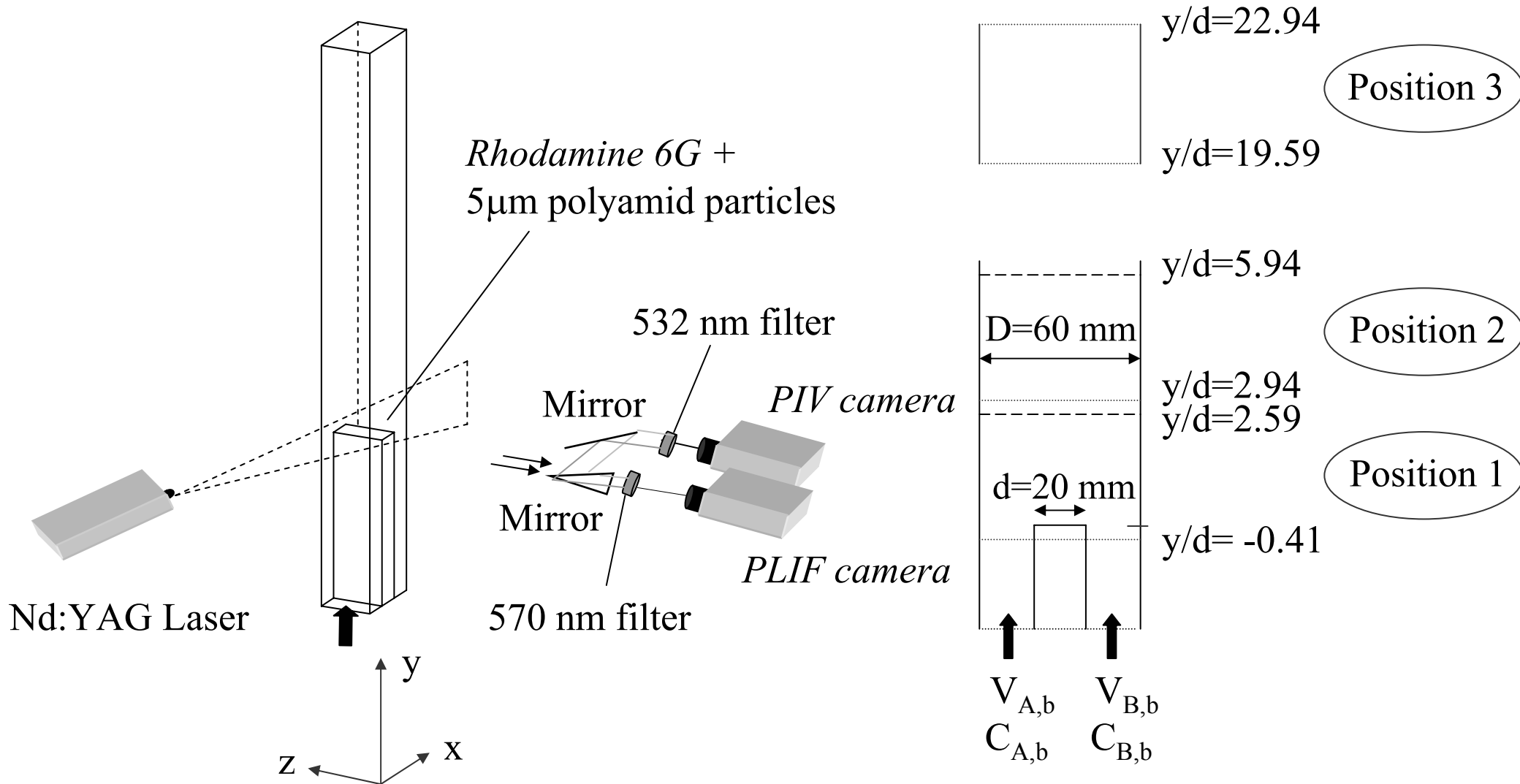
Flow Configuration

Confined wake flow

- Channel dimensions
 - Mixing channel
 - Length 640 mm
 - Cross-section 60 mm x 60 mm
 - Feed channel
 - Length 330
 - Cross-section 20 mm x 60 mm
- Flow conditions
 - Fluid : Water
 - Feed channel A : $V_{A,b} / V_{B,b} = 1, 0.5, 0.25$
 - Feed channel B : $Re_B = \rho V_{B,b} D_{h,B} / \mu = 5100$

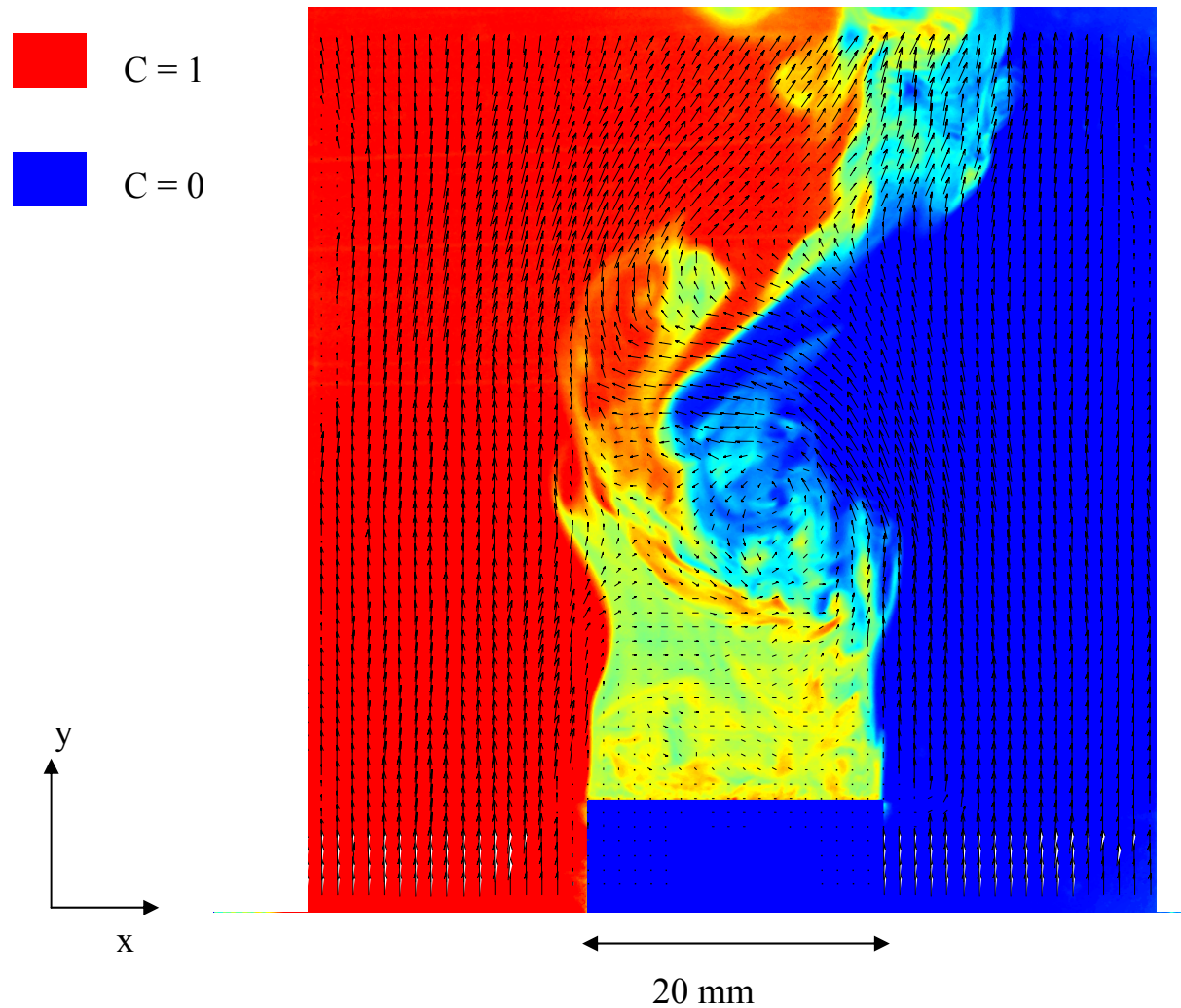


PIV/PLIF System

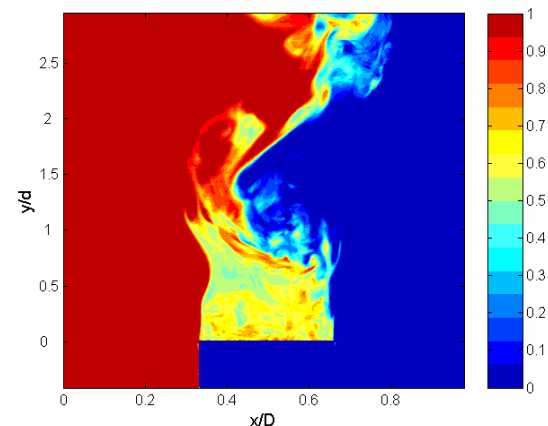
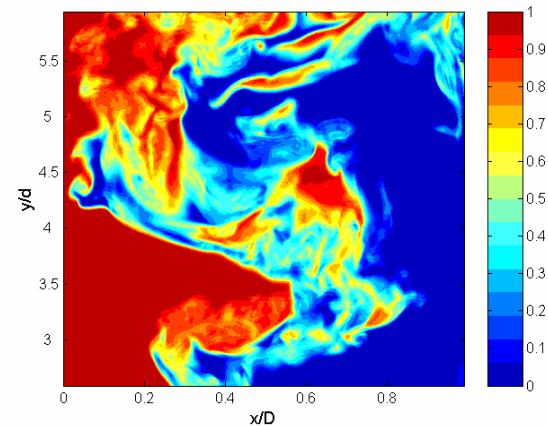
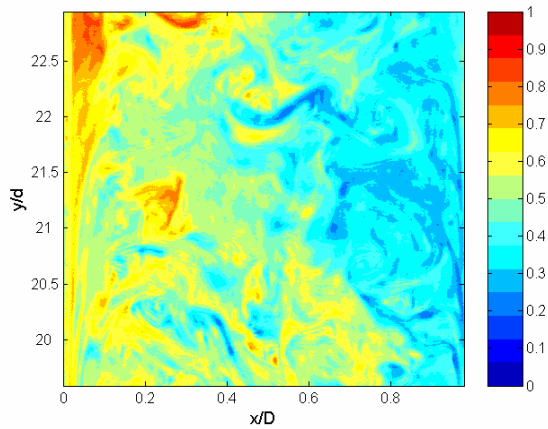




PIV/PLIF Measurements (1)

Instantaneous velocity and concentration



PIV/PLIF Measurements (2)



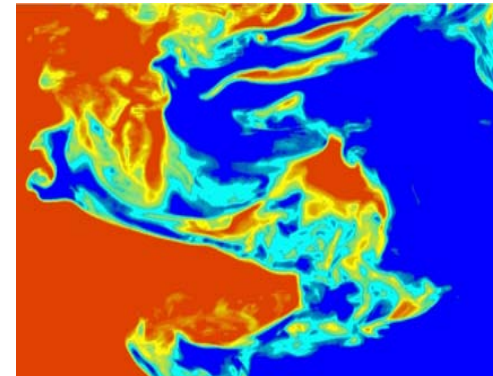
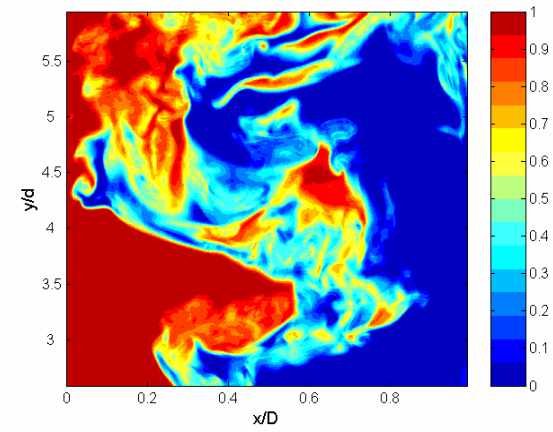
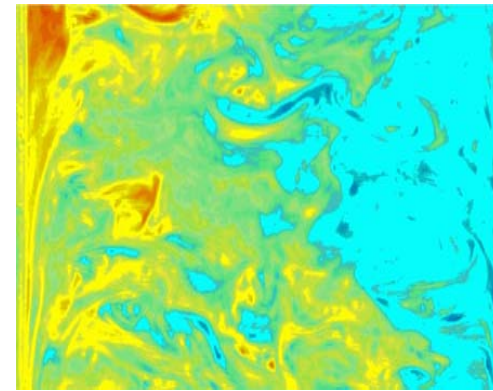
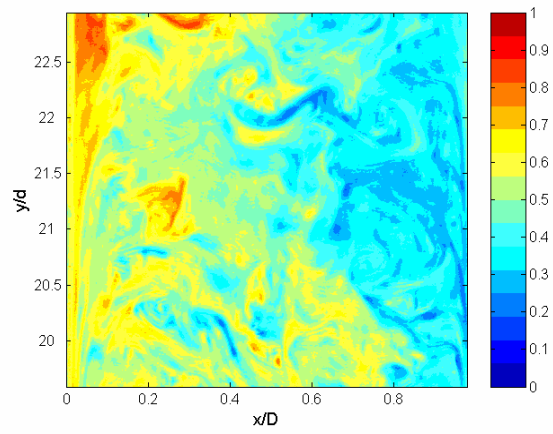
 $C = 1$
 $C = 0$



- Pure mixing experiment
 - Concentration of species A
 - High concentration ($C=1$) red
 - Low concentration ($C=0$) blue

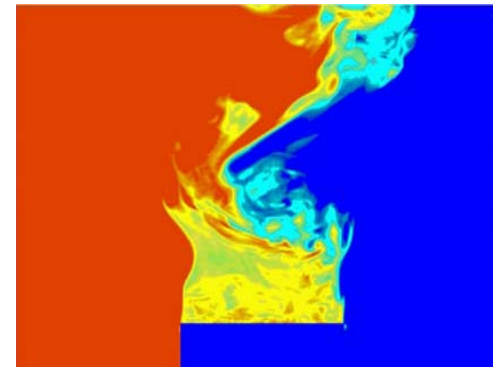
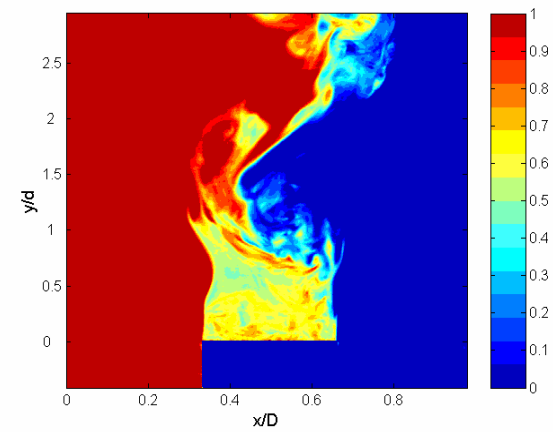
- Instantaneous images at three different heights

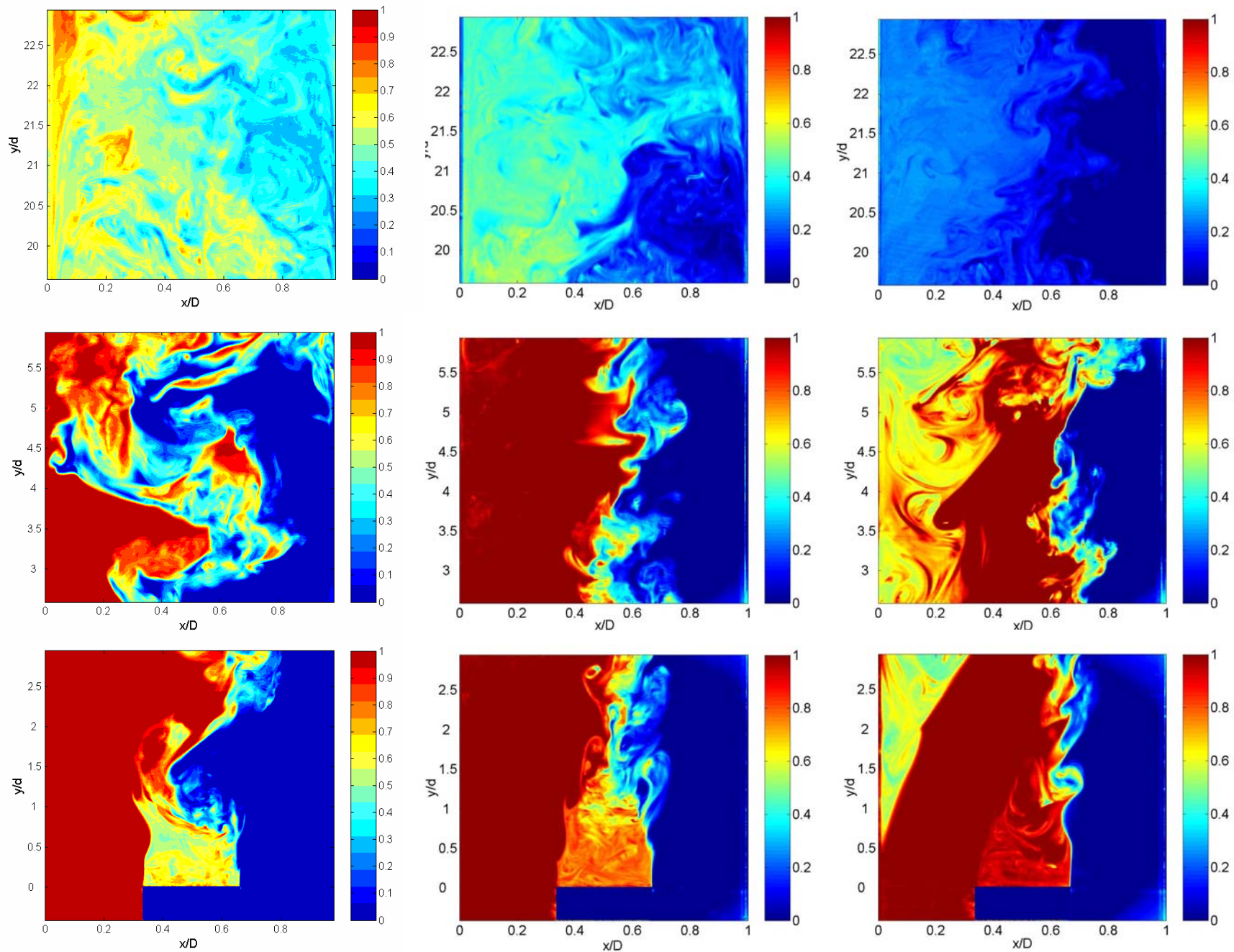
- Note heterogeneous structures

- Averages produced using 200 images



 $C = 1$
 $C = 0$





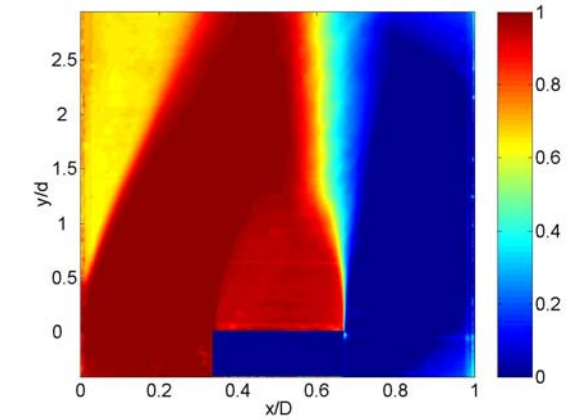
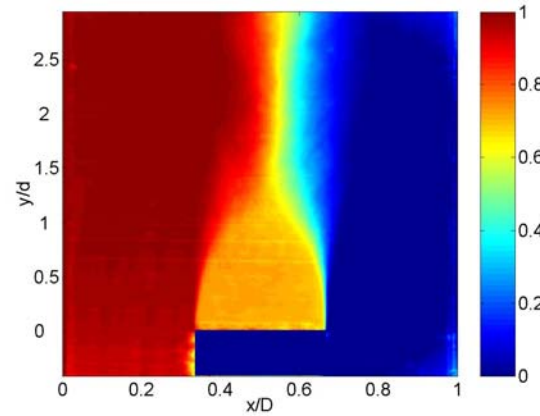
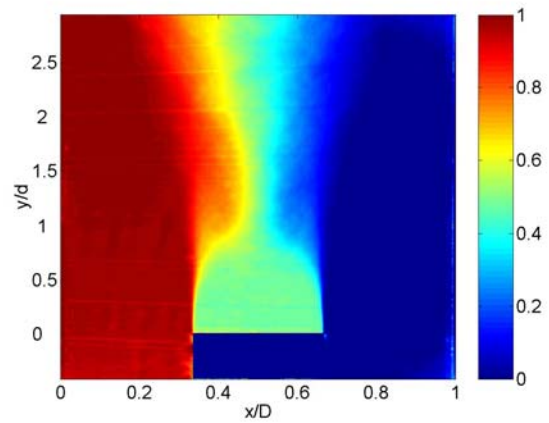
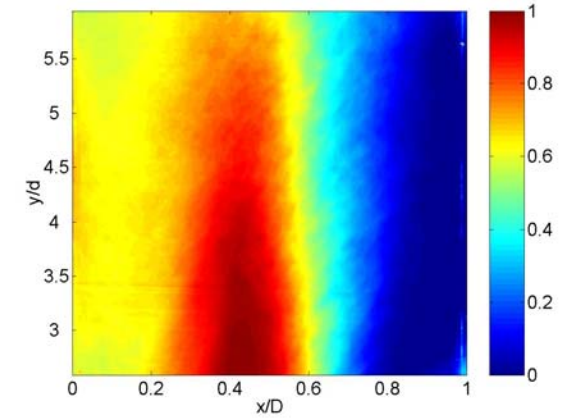
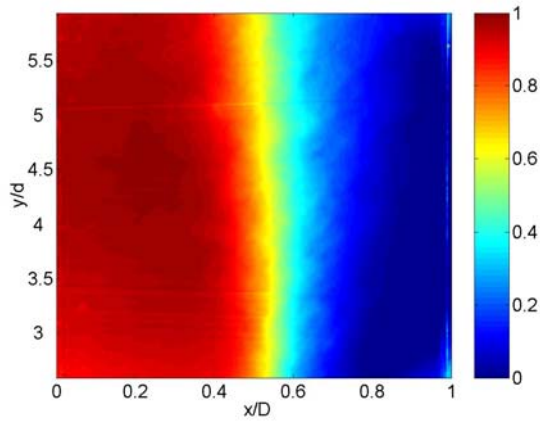
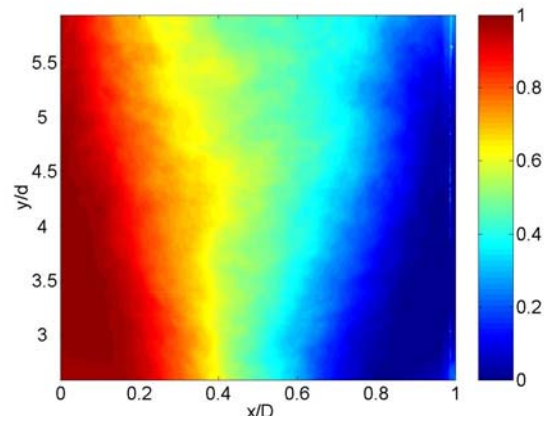
1:1

0.5:1

0.25:1

PIV/PLIF Measurements (3)

Mean concentrations



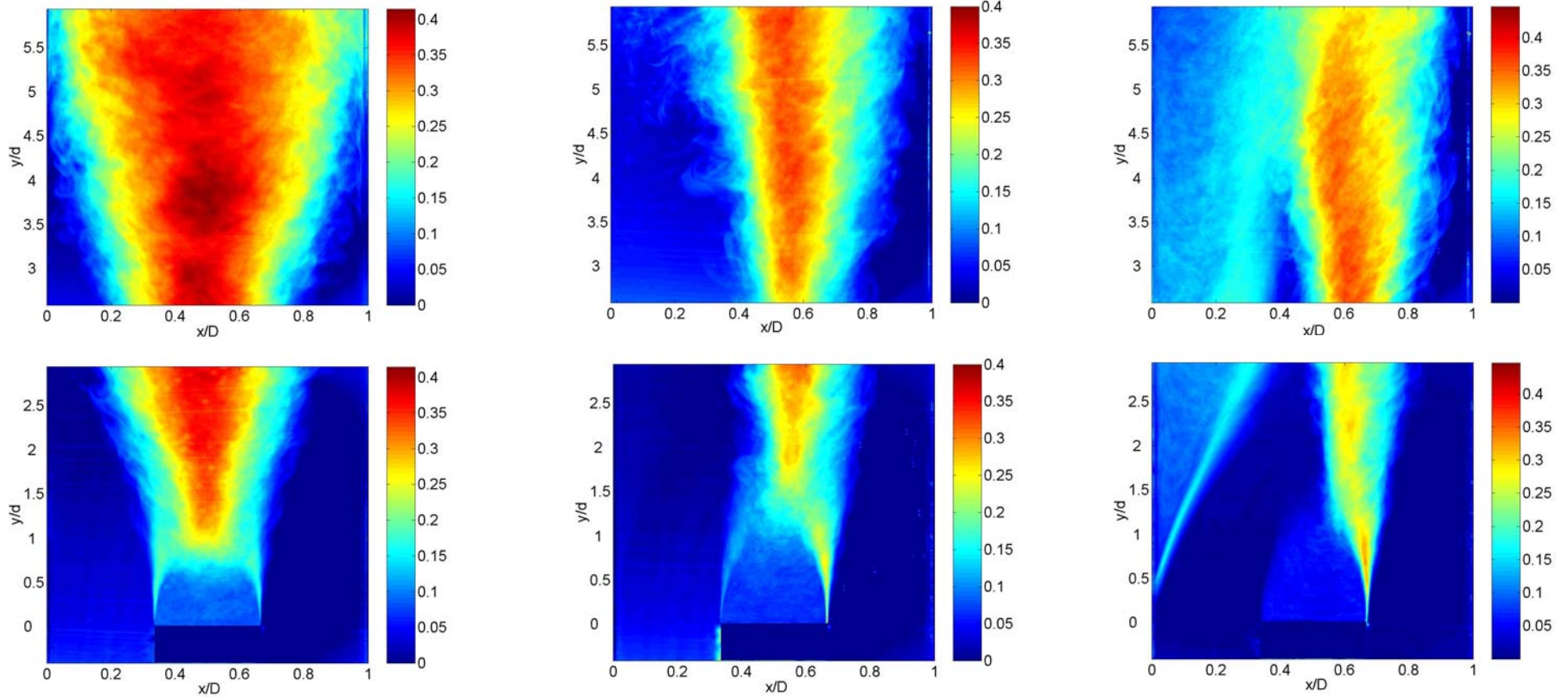
1:1

0.5:1

0.25:1

PIV/PLIF Measurements (4)

RMS concentrations



1:1

0.5:1

0.25:1

Conservation Equations

Mass

$$\frac{\partial U_j}{\partial x_j} = 0$$

Momentum

$$\frac{\partial}{\partial x_j} (\rho U_j U_i) = -\frac{\partial p}{\partial x_j} + \frac{\partial \tau_{ij}}{\partial x_j}; \quad \tau_{ij} = (\mu + \mu_T) \cdot \left[\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right] - \frac{2}{3} \delta_{ij} \cdot \rho k$$

Mixture fraction

$$\phi = C / C_{A,b}$$

$$\frac{\partial}{\partial x_j} (\rho U_j \phi) = \frac{\partial}{\partial x_j} \left(\Gamma_\phi \frac{\partial \phi}{\partial x_j} \right); \quad \Gamma_\phi = \frac{\mu}{Sc_\phi} + \frac{\mu_T}{Sc_T}$$



Turbulence and mixing models

Turbulence Models

- Standard k - ε model
- *RNG* k - ε model
- Chen-Kim k - ε model

Micromixing model

- Multi-peak presumed PDF model (Fox 1998)

Multi-Peak PDF Model (1)

Presumed PDF

$$f_{\phi}(\psi; x, t) = \sum_{n=1}^{N_p} p_n(x, t) \delta(\psi - \phi_n(x, t))$$

Transport equation for probability p_n

$$\frac{\partial}{\partial t}(\rho p_n) + \frac{\partial}{\partial x_j}(\rho U_j p_n) = \frac{\partial}{\partial x_j} \left(\Gamma_T \frac{\partial p_n}{\partial x_j} \right) + G_n(p)$$

Transport equation for probability-weighted concentration s_n

$$\frac{\partial}{\partial t}(\rho s_n) + \frac{\partial}{\partial x_j}(\rho U_j s_n) = \frac{\partial}{\partial x_j} \left(\Gamma_T \frac{\partial s_n}{\partial x_j} \right) + M_n(p, s)$$

- Conservation relations $\sum_{n=1}^{N_p} p_n = 1; \quad \sum_{n=1}^{N_p} G_n = 0; \quad \sum_{n=1}^{N_p} M_n = 0$

Multi-Peak PDF Model (2)

Local concentration in environment/peak n

$$\phi_n = \frac{S_n}{P_n}$$

Mean concentration

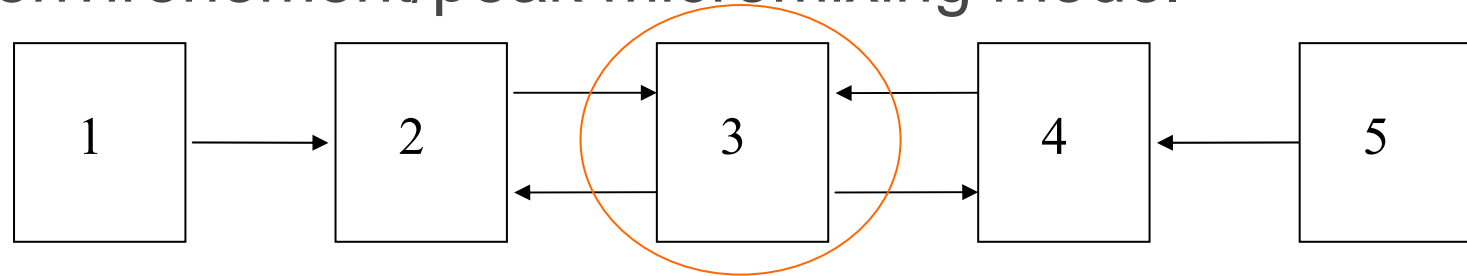
$$\langle \phi \rangle = \sum_{n=1}^{N_p} P_n \phi_n = \sum_{n=1}^{N_p} S_n$$

Variance of concentration fluctuations

$$\langle \phi'^2 \rangle = \sum_{n=1}^{N_p} P_n \phi_n^2 - \langle \phi \rangle^2$$

Multi-Peak PDF Model (3)

Five environment/peak micromixing model



Inlet stream 1:

$$\phi_1 = 1$$

$$p_1 = 1$$

$$\phi_2 < 1$$

$$1 > \phi_3 > 0$$

$$\phi_4 > 0$$

Inlet stream 2:

$$\phi_5 = 0$$

$$p_5 = 1$$

Typical modelling of G_n and M_n for environment/peak 3

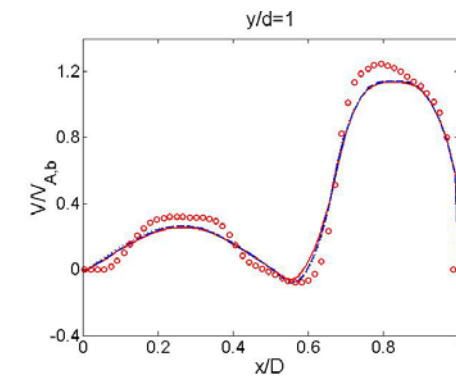
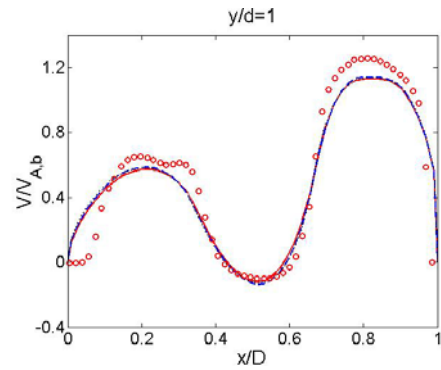
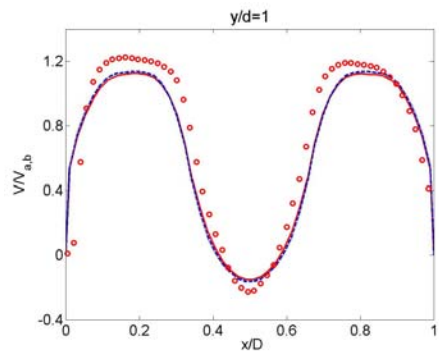
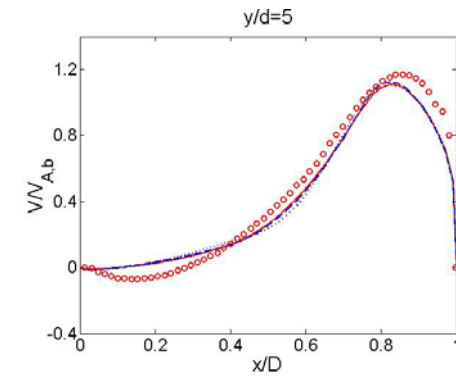
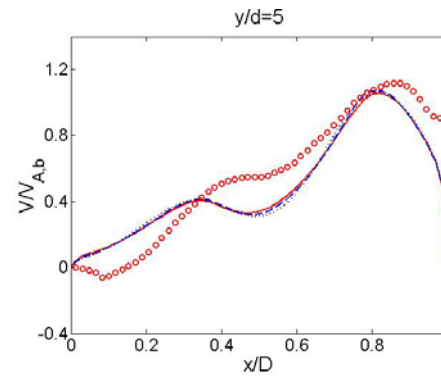
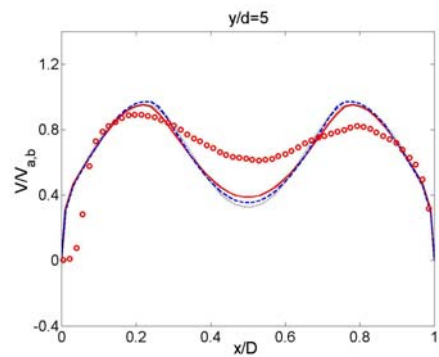
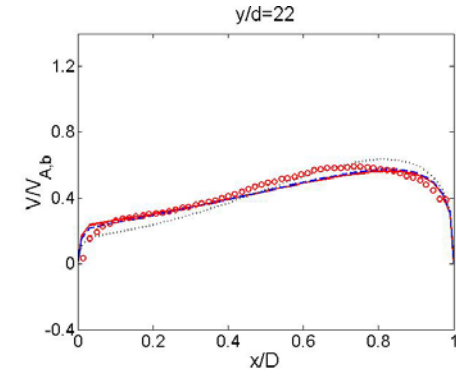
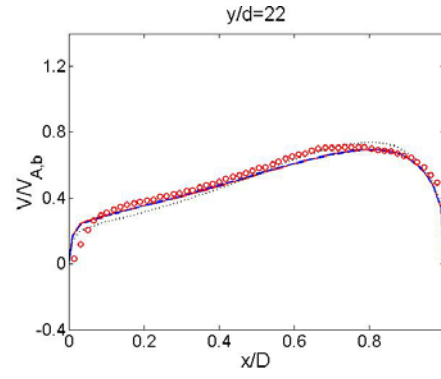
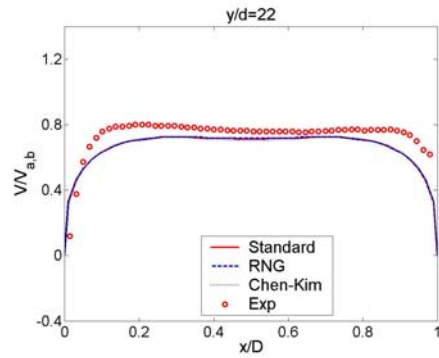
$$G_3 = r_2 + r_4 - 2r_3; \quad M_3 = r_2 \phi_2 + r_4 \phi_4 - 2r_3 \phi_3$$

- Probability fluxes

$$r_n = \gamma p_n$$

- Rate of micromixing $\gamma = \frac{1}{\tau_m}$; $\tau_m = \frac{1}{C_\phi} \frac{k}{\varepsilon}$; $C_\phi = 1.0$

Mean Axial Velocity (V)

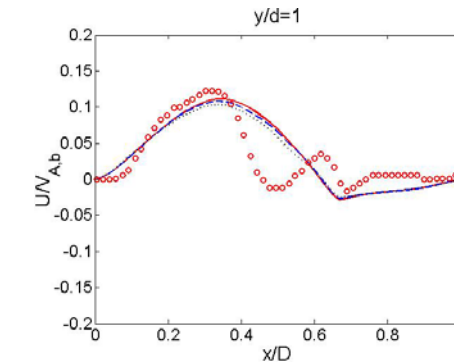
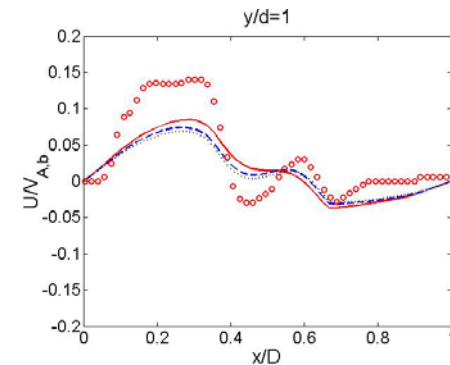
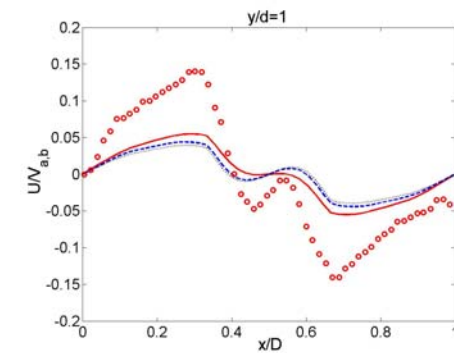
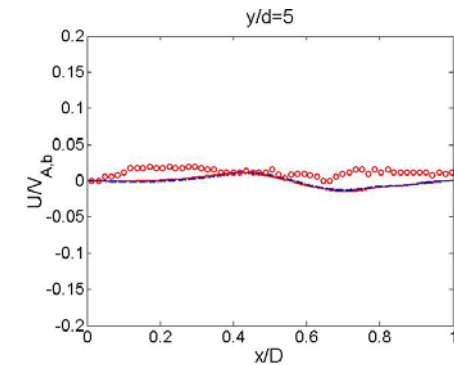
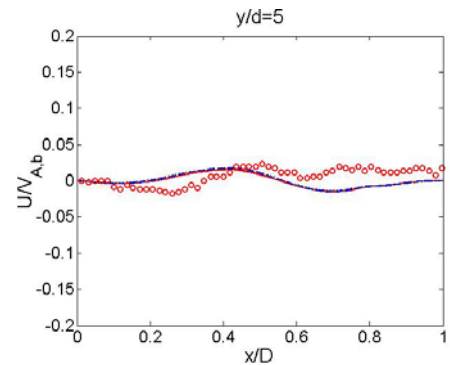
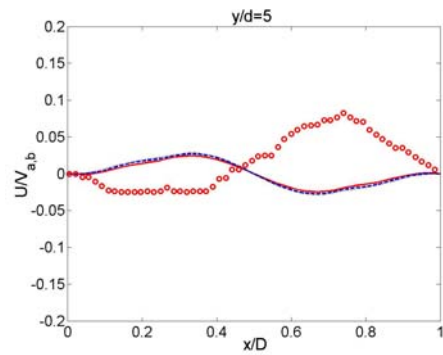
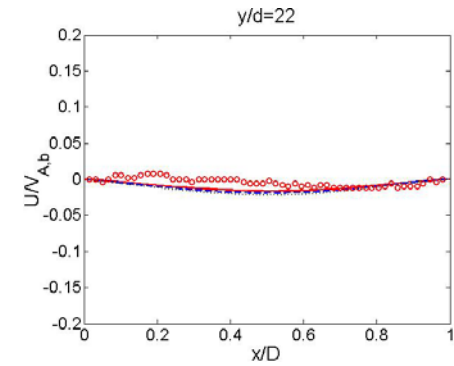
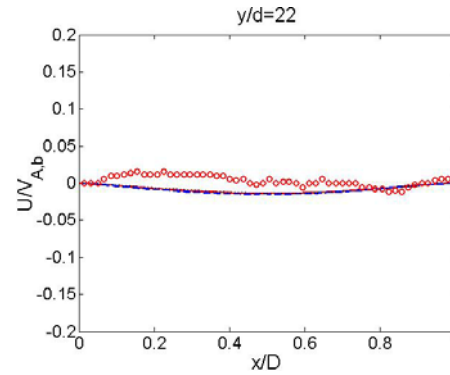
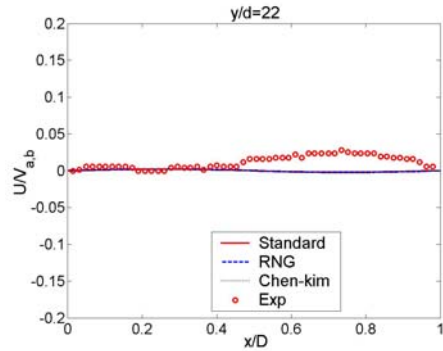


1:1

0.5:1

0.25:1

Mean Transverse Velocity (U)

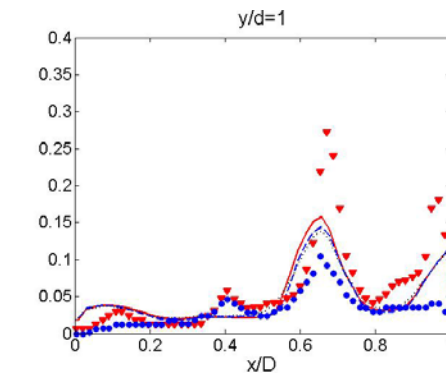
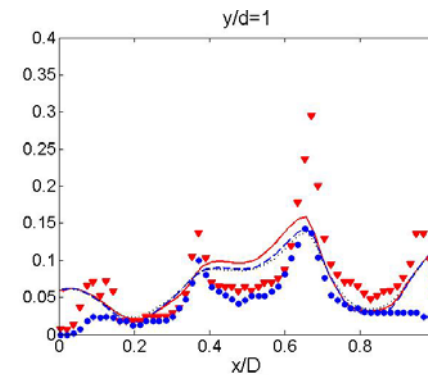
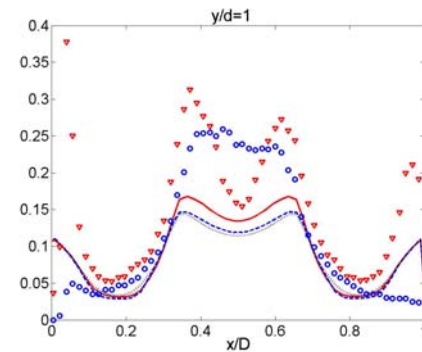
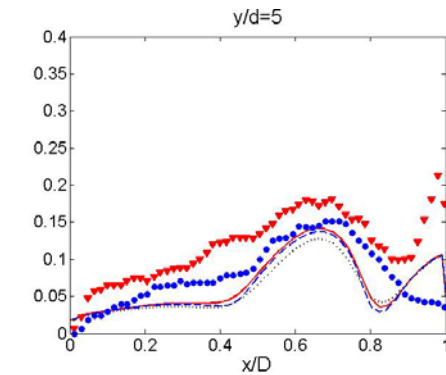
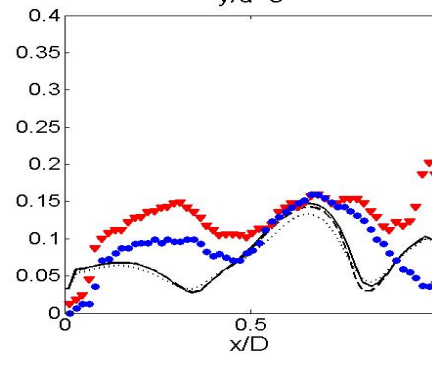
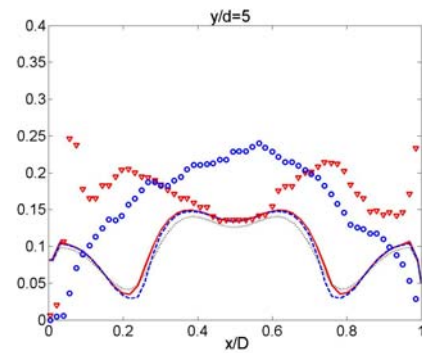
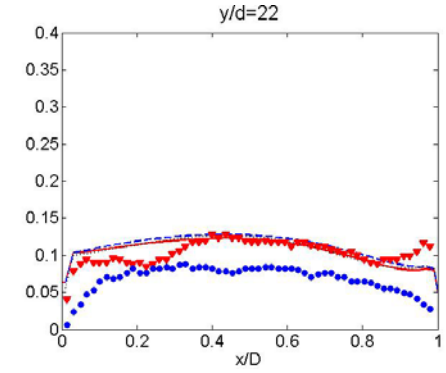
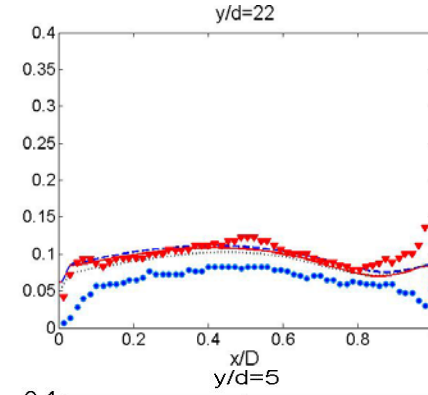
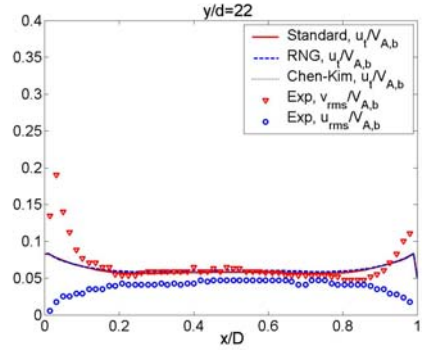


1:1

0.5:1

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Turbulence Velocities



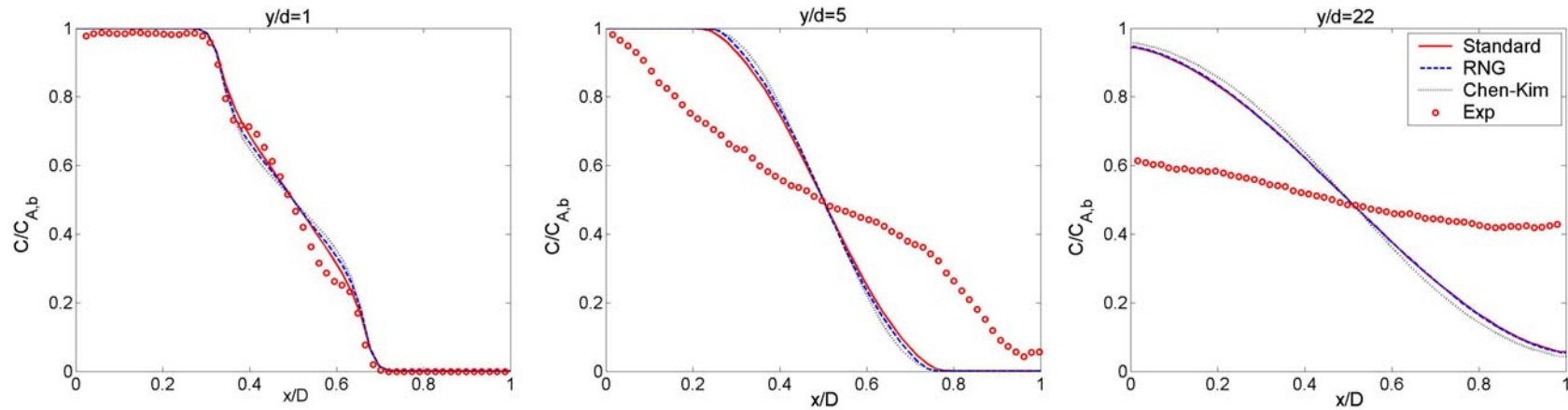
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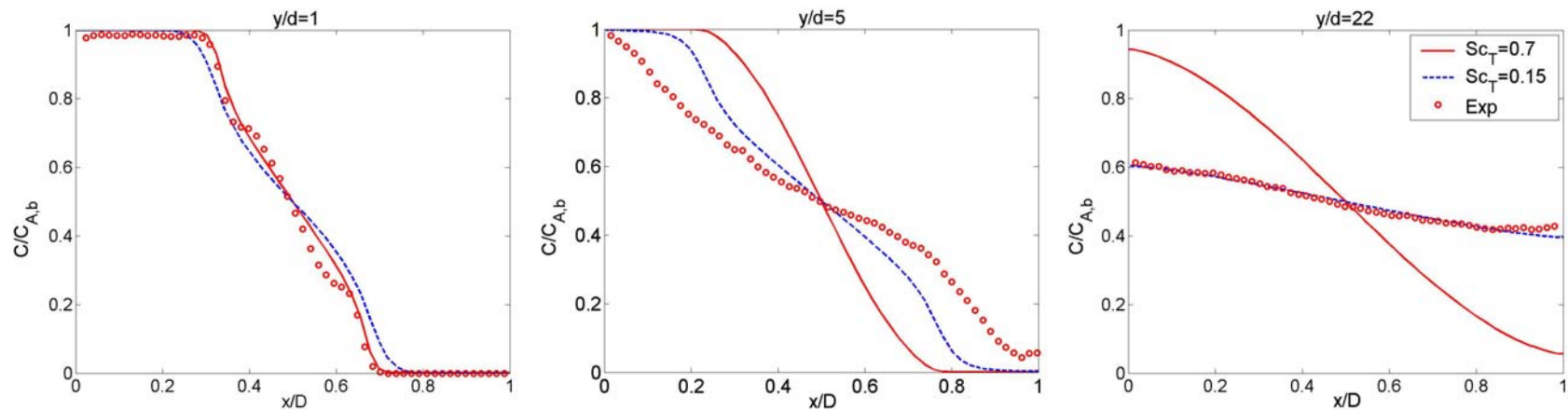
0.25:1

Mean Concentration

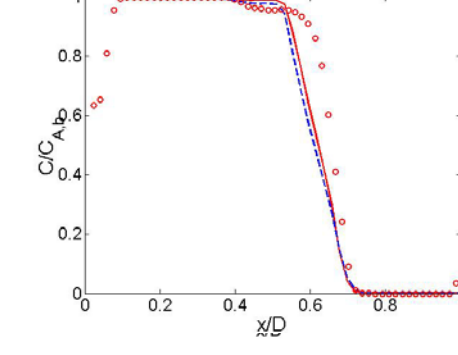
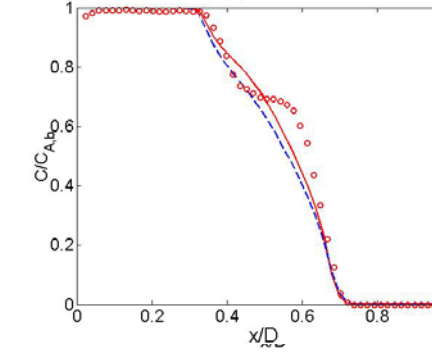
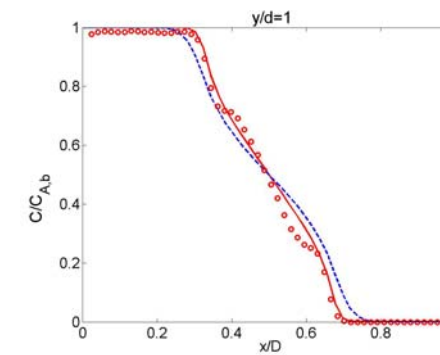
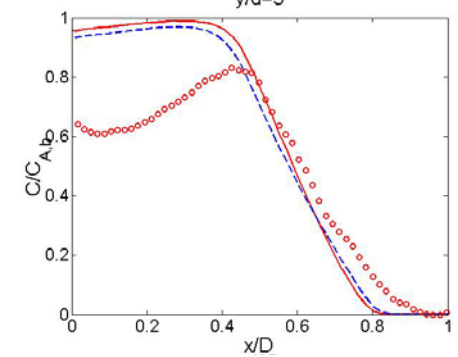
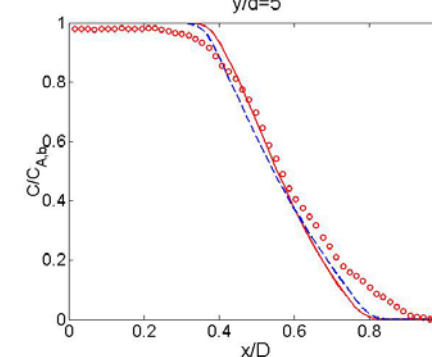
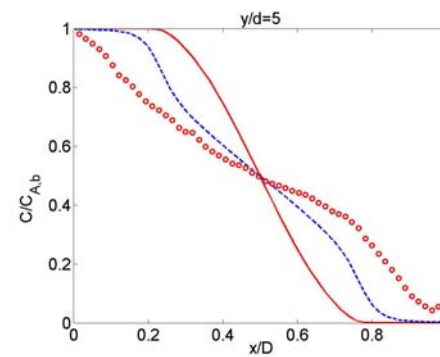
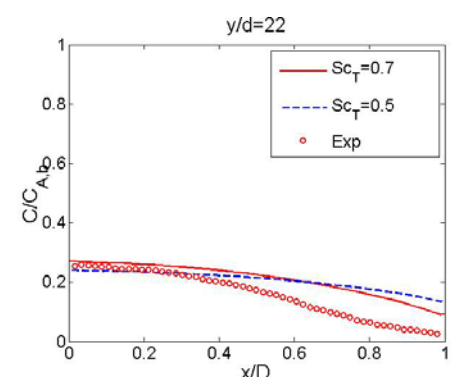
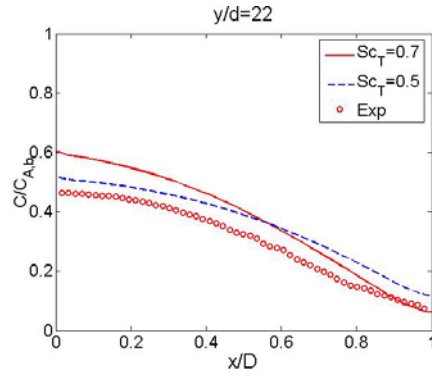
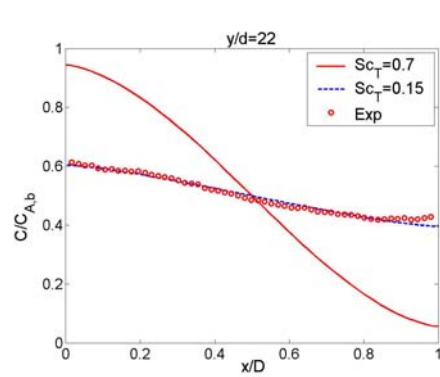
Turbulence models; 1:1 case



Turbulent Schmidt number; 1:1 case



Mean Concentration

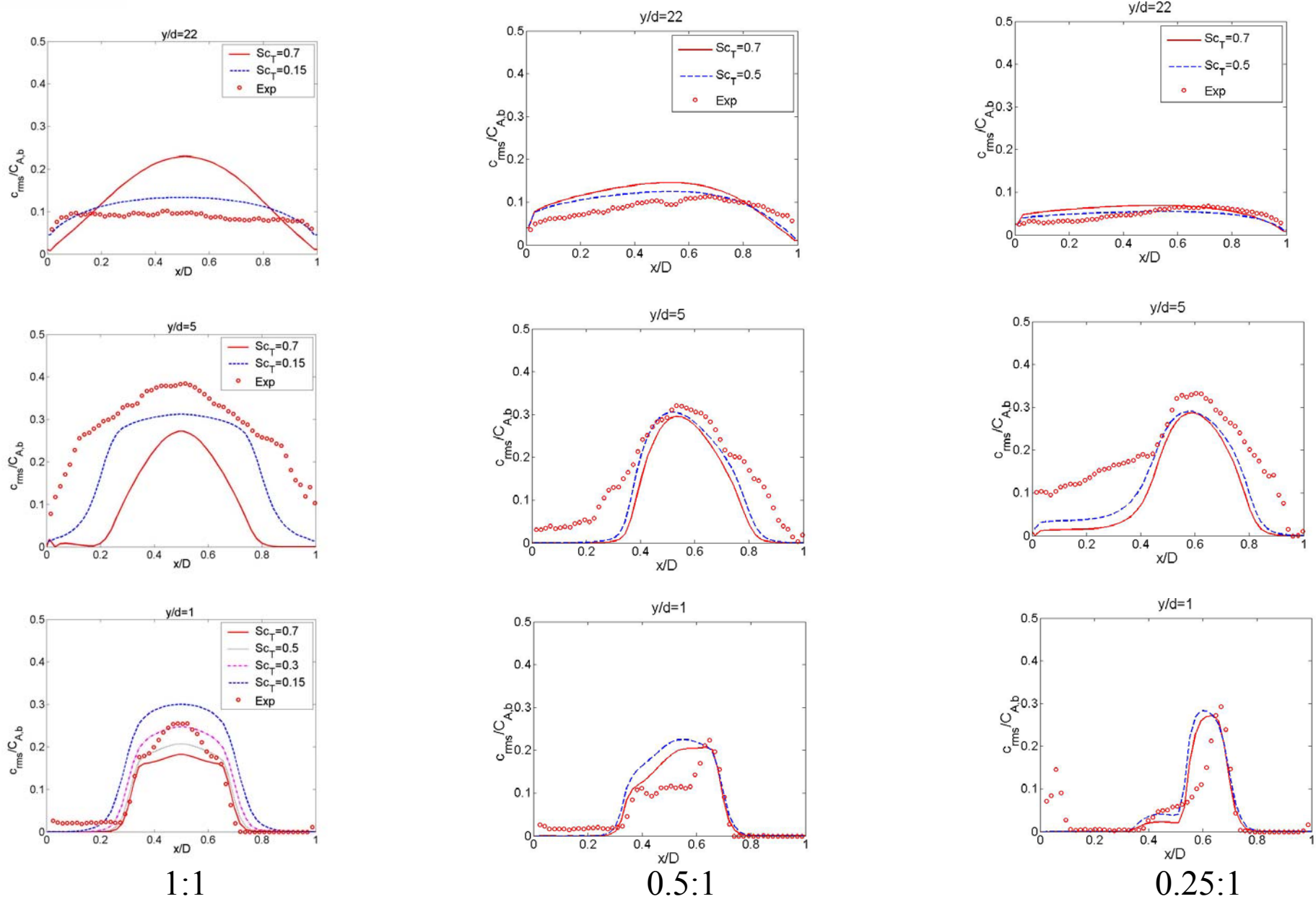


1:1

0.5:1

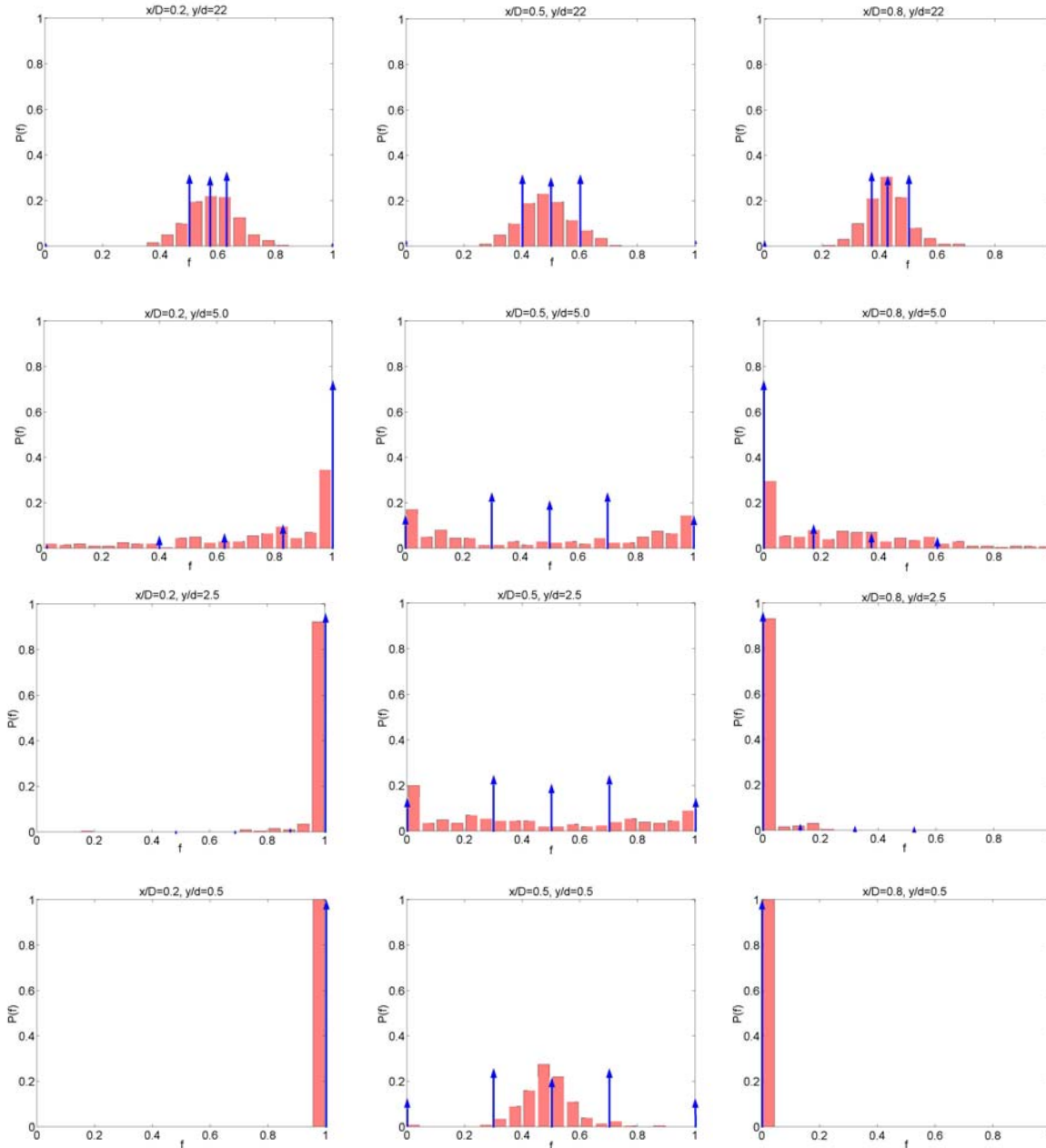
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Concentration Fluctuations



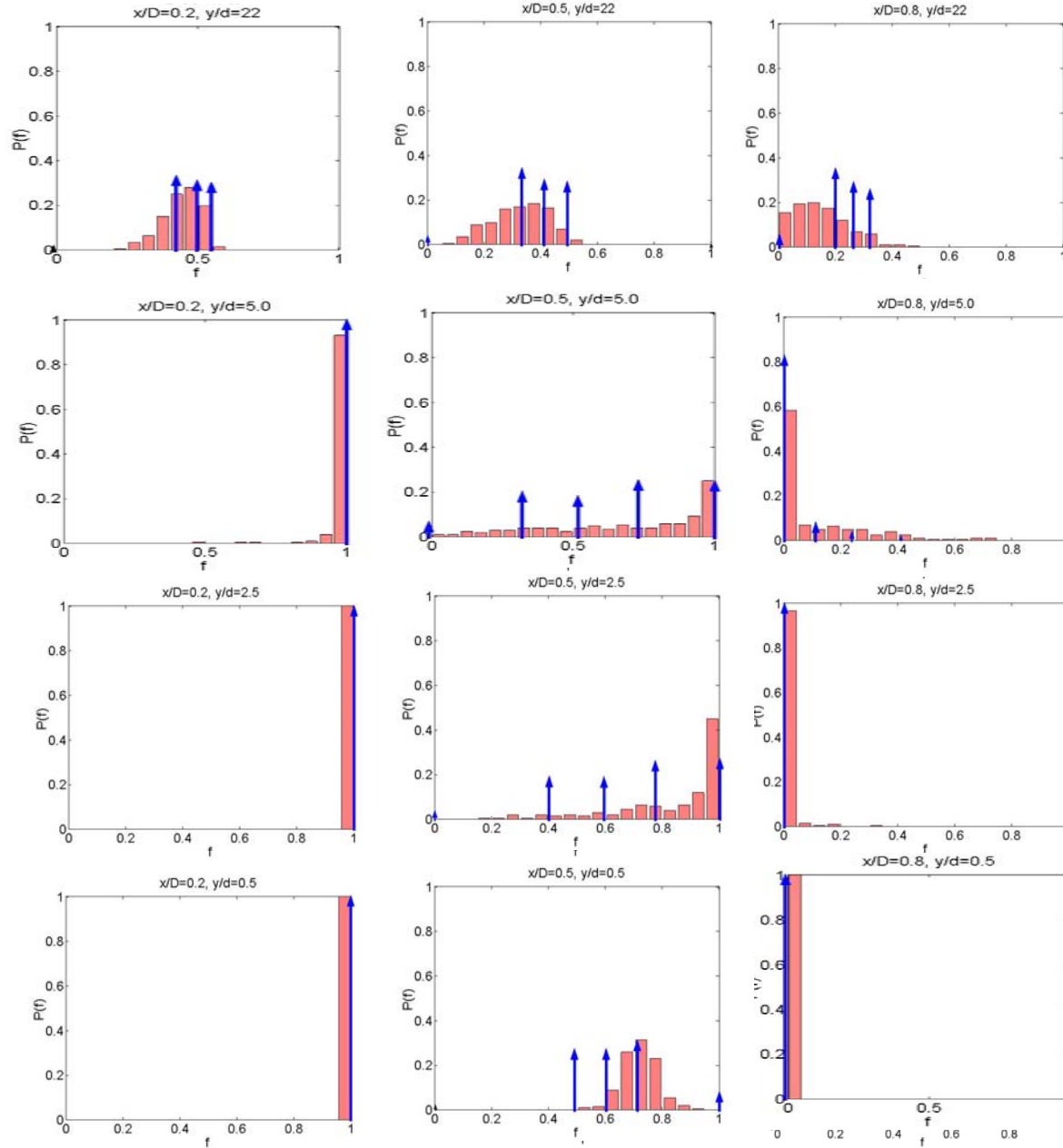
Five-peak presumed PDF model 1:1

Probability Density Functions



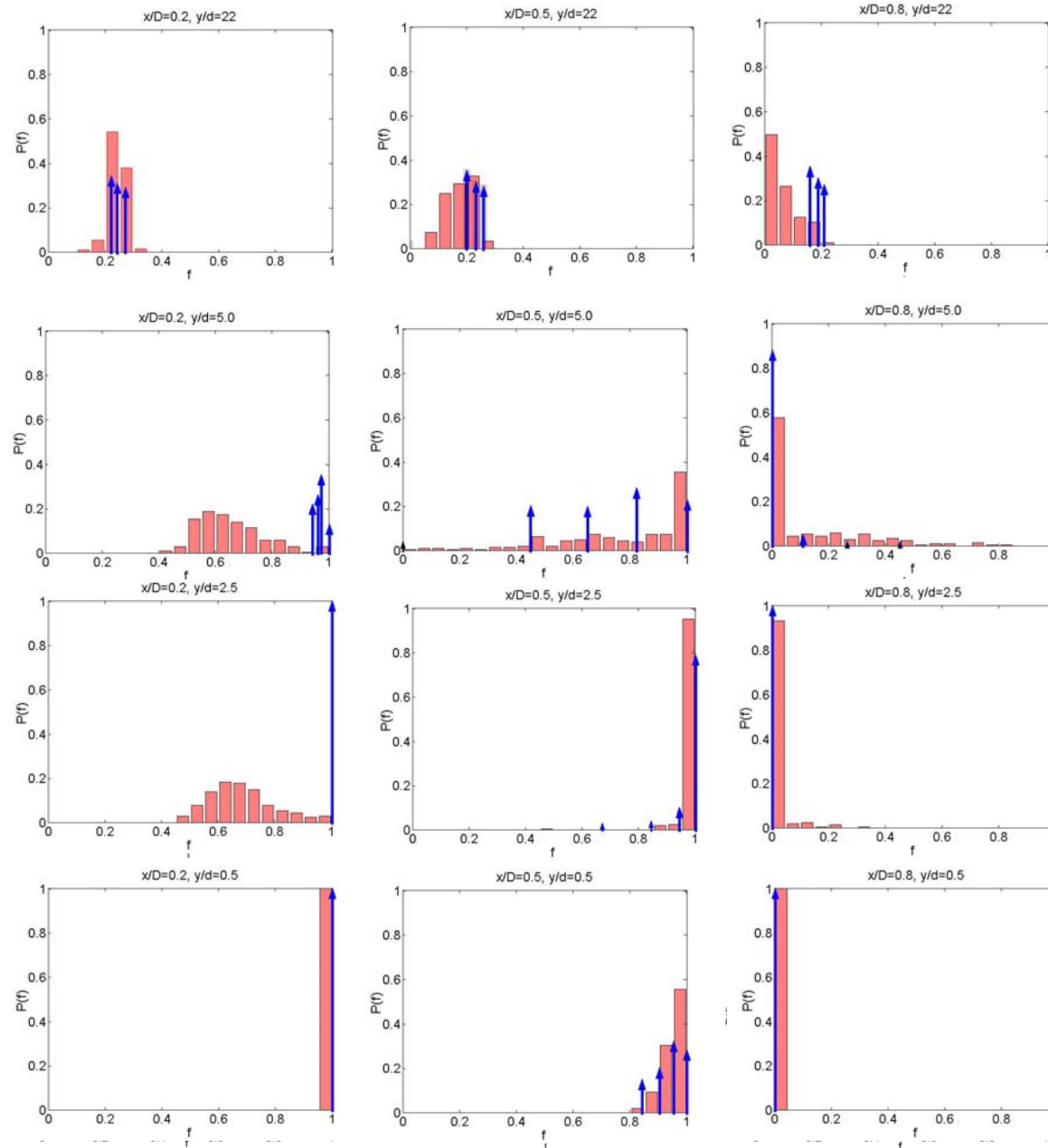
Five-peak presumed PDF model 0.5:1

Probability Density Functions



Five-peak presumed PDF model 0.25:1

Probability Density Functions



Overall mixing characteristics

- Coefficient of variation => Measure of macromixing

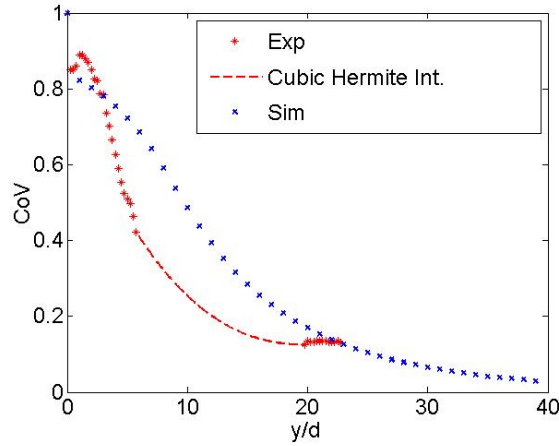
$$\text{CoV} = \frac{\sqrt{\frac{\sum_{i=1}^N (C_i - \langle C \rangle_A)^2}{N-1}}}{\langle C \rangle_A} \quad A\text{-area}$$

- Decay function => Measure of micromixing

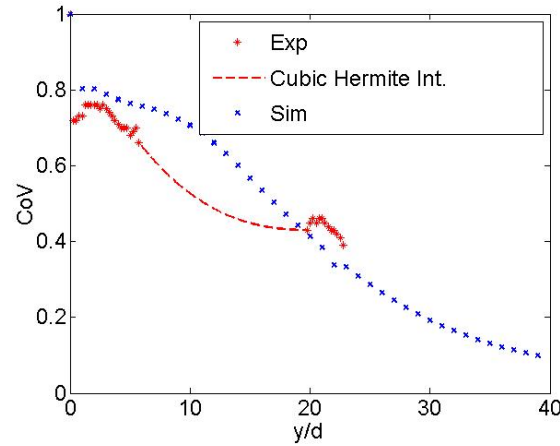
$$d = \frac{\langle c_{rms} \rangle_A}{\langle C \rangle_A}$$

Coefficient of variation (CoV) and decay function (d)

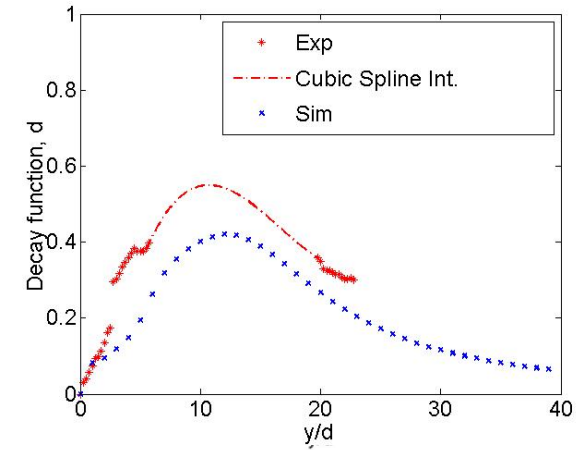
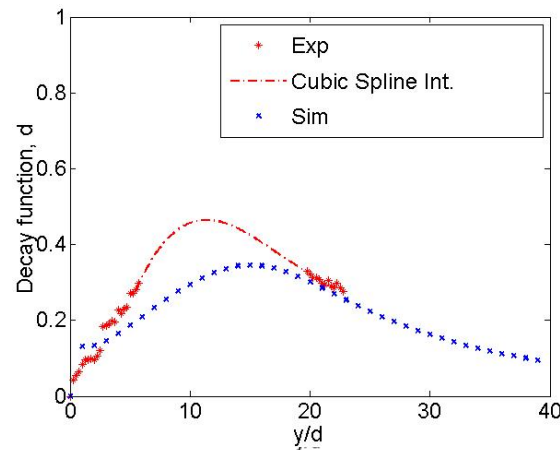
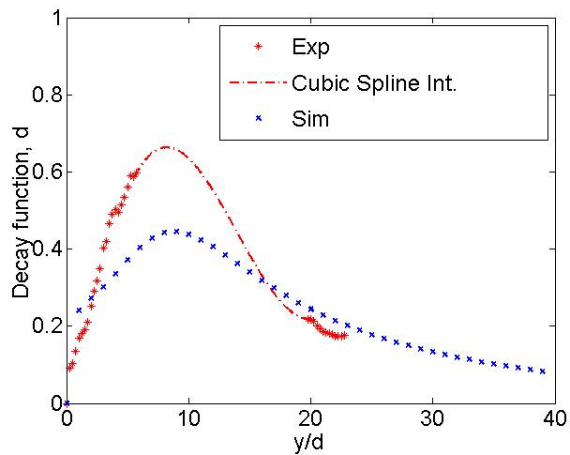
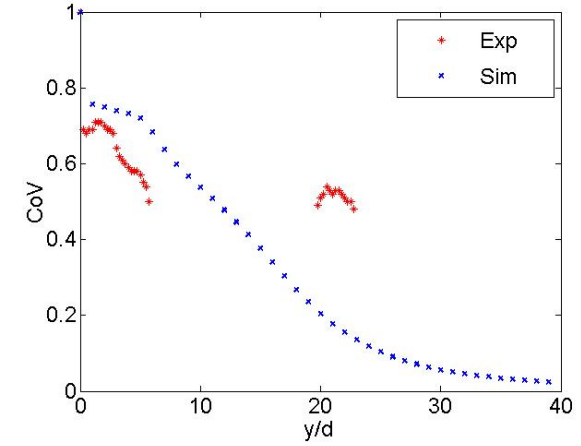
1:1



0.5:1



0.25:1



Concluding remarks (1)

- The different k - ε turbulence models do not manage to capture the correct recovery from wake to channel flow, especially for the 1:1 case
- The defects in the flow modelling also transfers to the mixing predictions
- A reduction of the turbulent Schmidt number (0.15 for 1:1 case and 0.5-0.7 for the other) is needed to achieve good predictions of both mean and rms concentrations
- The five-peak presumed PDF model predicts the streamwise decay of micromixing reasonably correct

Concluding remarks (2)

- The concentration PDF's are reasonably predicted by the five-peak presumed PDF model
- The overall mixing characteristics (CoV and decay function) are reasonably predicted
- A LES turbulence model is probably required to improve the flow modeling
- Solution of the multi-peak PDF method should use the direct quadratic method of moment (DQMOM) technique